



**Diffusion Fundamentals VI**  
**Spreading in Nature,**  
**Technology and Society**  
**Dresden, August 2015**  
**Pre-School**

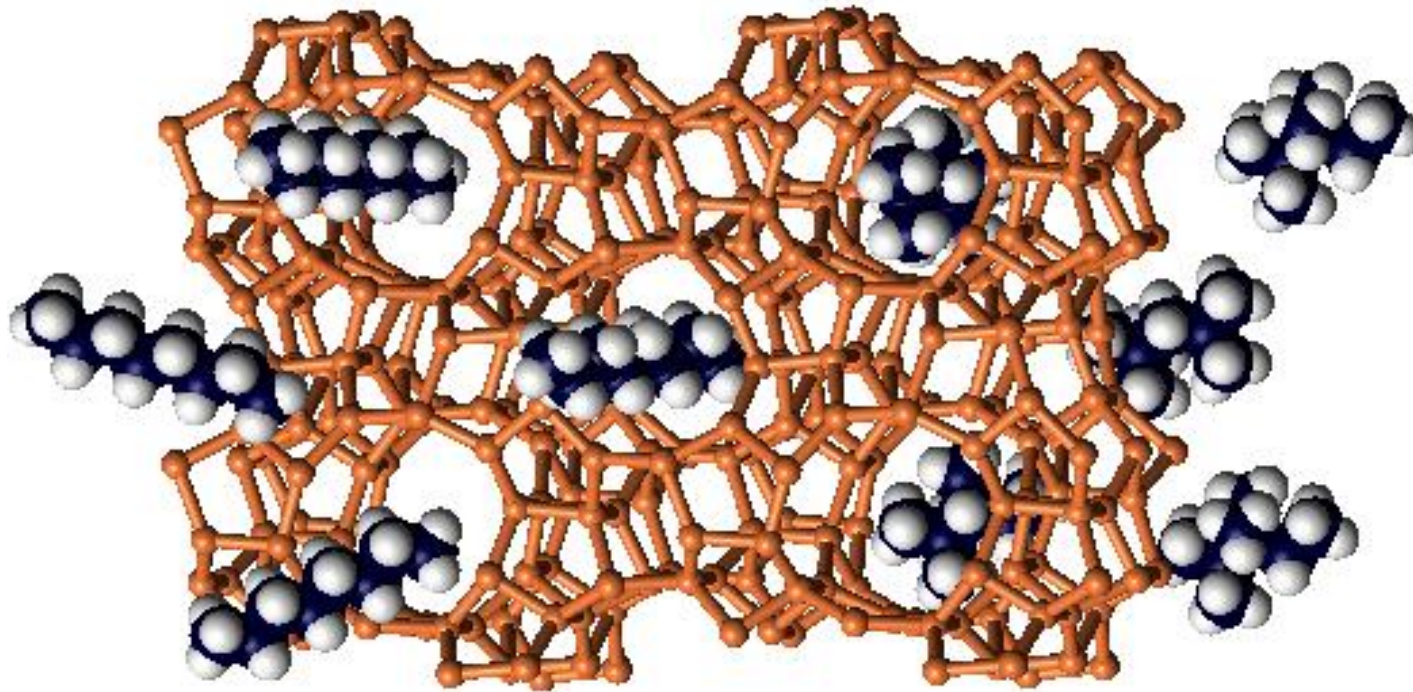


**Diffusion Step by Step:**  
**Looking at Molecules in Pore Networks**

**Jörg Kärger**

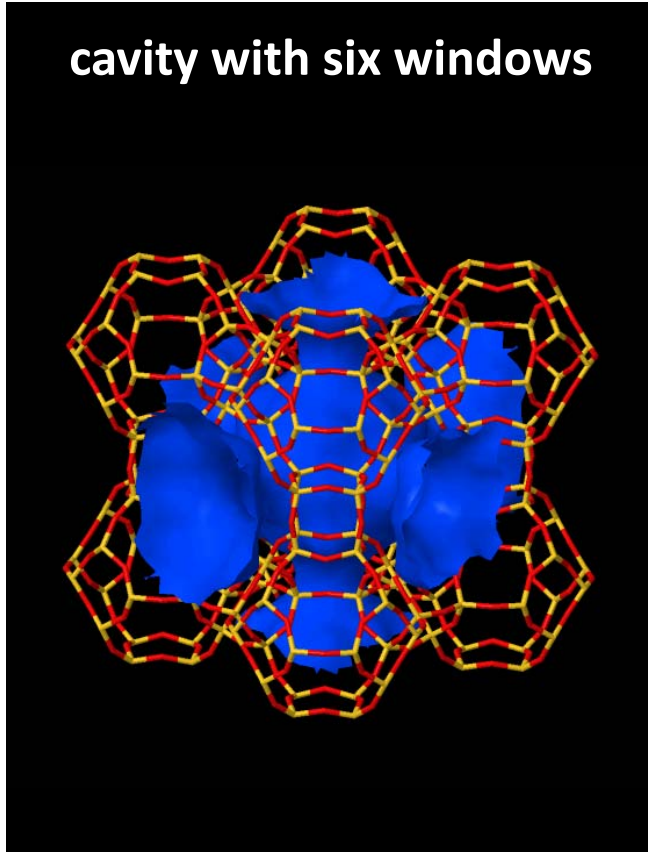
**University of Leipzig**  
**Faculty of Physics and Earth Sciences**  
**Institute of Experimental Physics**

**The system under study:  
Molecules in nanoporous materials**

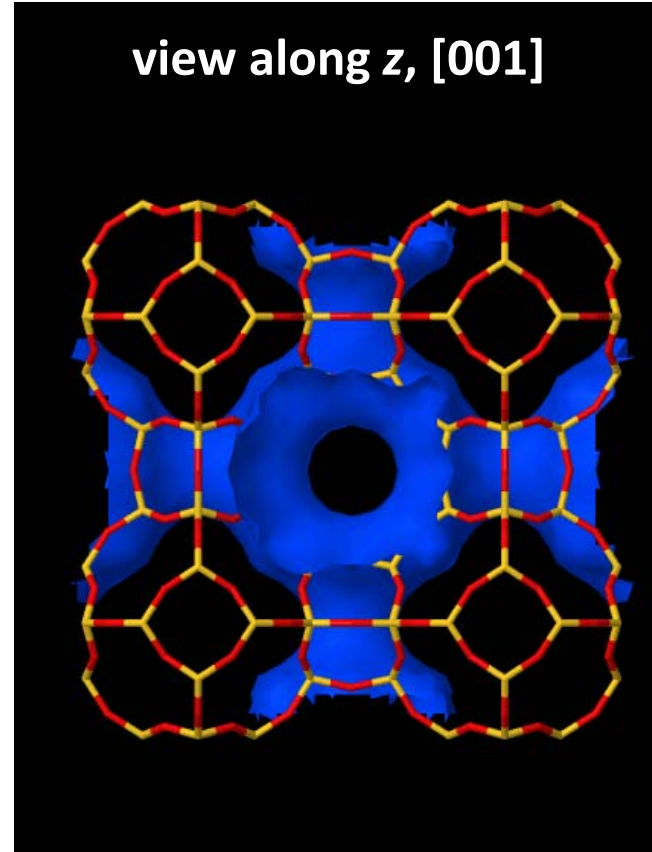


# LTA-type structure – cages/narrow windows (3d)

cavity with six windows

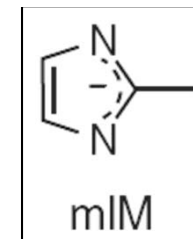


view along z, [001]

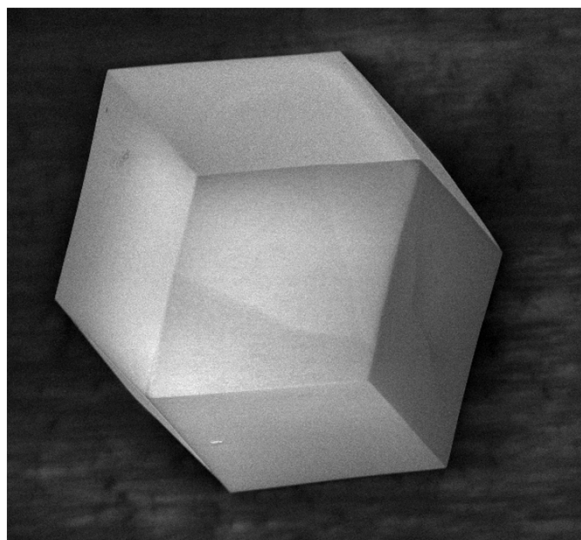


- large cavity (11 Å) framed by six narrow windows ( $4.1 \times 4.1 \text{ \AA}^2$ )

**MOFs (Metal-Organic Frameworks) of type ZIF:  
Zeolitic Imidazolate Frameworks (ZIF-8 ↔ SOD)**

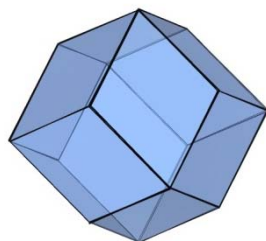


**SEM image (J. Caro)**

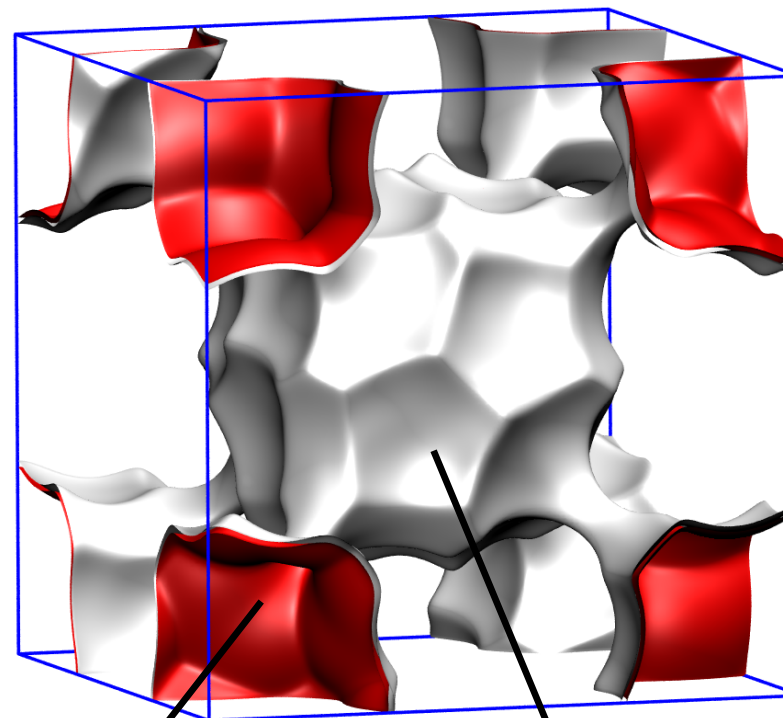


crystal size: up to 300  $\mu\text{m}$

crystal shape: rhombic  
dodecahedron



**potential landscape (R. Krishna)**



window size:  
ca. 3.4  $\text{\AA}$

cavity size: ca. 12  $\text{\AA}$

unit cell:  $a = b = c \approx 17 \text{\AA}$

**in collaboration with J. Caro, Hannover**



# Introducing into Spreading Fundamental by Looking at Molecules („Guests“) in Nanoporous Materials („Hosts“)

## The Benefit of Considering

**Molecules** as the object of spreading:

- observations with a **large number of diffusants**
- all diffusants („guests“) are **identical**
- diffusants **do not change** their properties with time

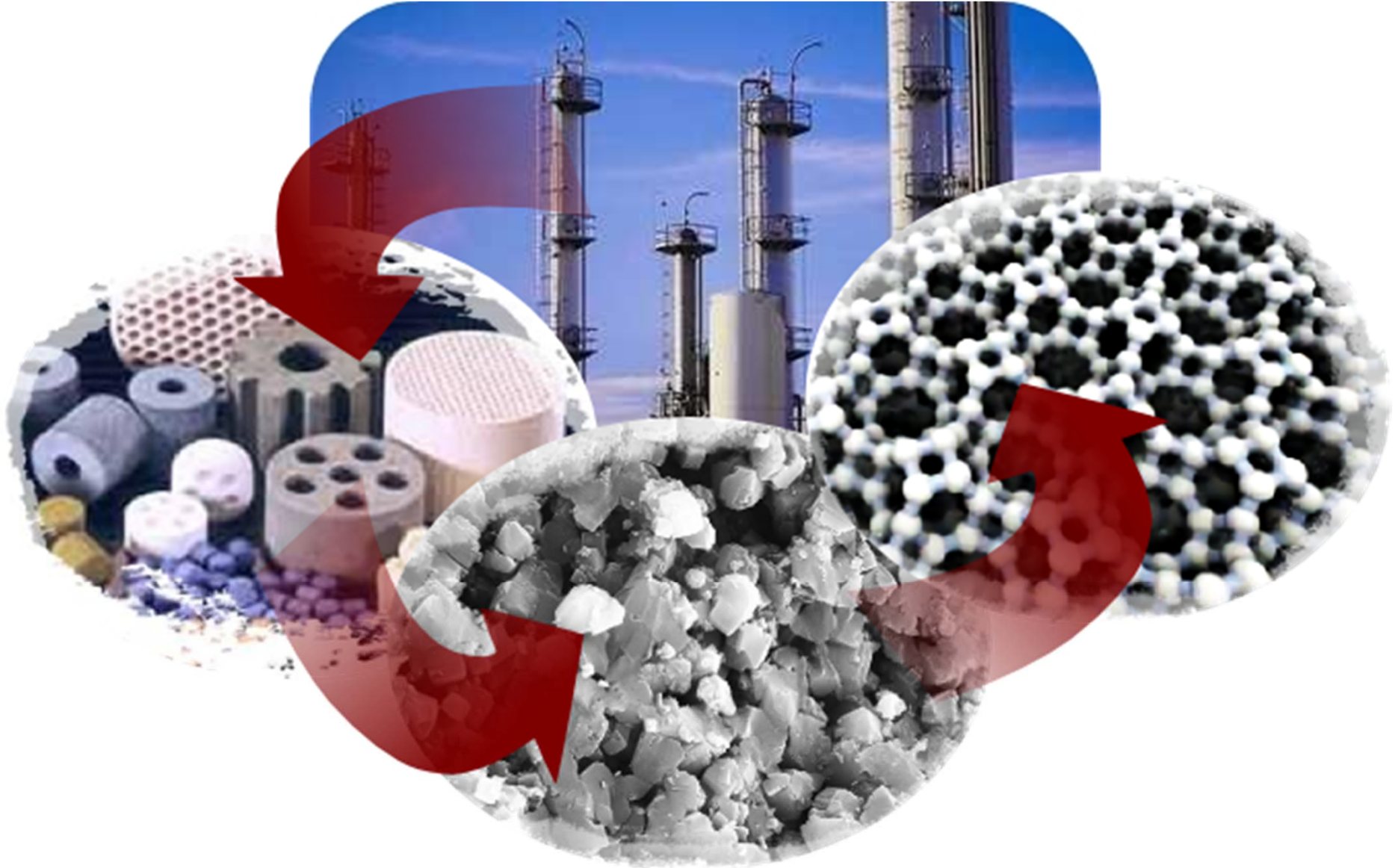
**Nanoporous Materials** as a host system:

- **well-defined conditions** for guest movement
- option of **deliberate variation** of these conditions

## Enabling

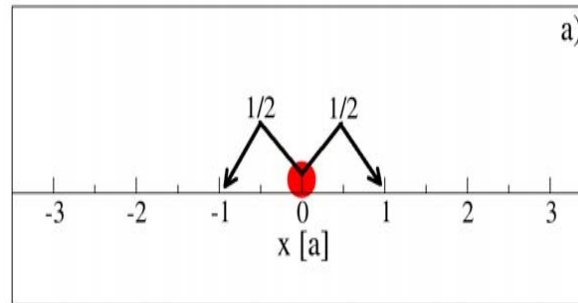
- High **statistical relevance**
- Vast options for **varying initial and boundary conditions**
- High **reproducibility** of measurement
- Hope for „**simple**“ **relations** and predictability

## Last not Least: Systems of High Technological Relevance



**Nanoporous materials are key to many value-adding processes,  
their performance is controlled by the rate of DIFFUSION**

# What we have to keep in mind from lesson 1: Probability distribution



$$P_n(m) = \frac{1}{2} P_{n-1}(m-1) + \frac{1}{2} P_{n-1}(m+1), \quad t = n\tau, \quad x = ma, \quad P_n(m) = aP(x, t)$$

$$P(x, t) = \frac{1}{2} P(x-a, t-\tau) + \frac{1}{2} P(x+a, t-\tau)$$

$$P(x, t) - P(x, t-\tau) = \frac{1}{2} P(x-a, t-\tau) + \frac{1}{2} P(x+a, t-\tau) - P(x, t-\tau)$$

$$\frac{P(x, t) - P(x, t-\tau)}{\tau} = \frac{a^2}{2\tau} \frac{P(x-a, t-\tau) + P(x+a, t-\tau) - 2P(x, t-\tau)}{a^2}$$

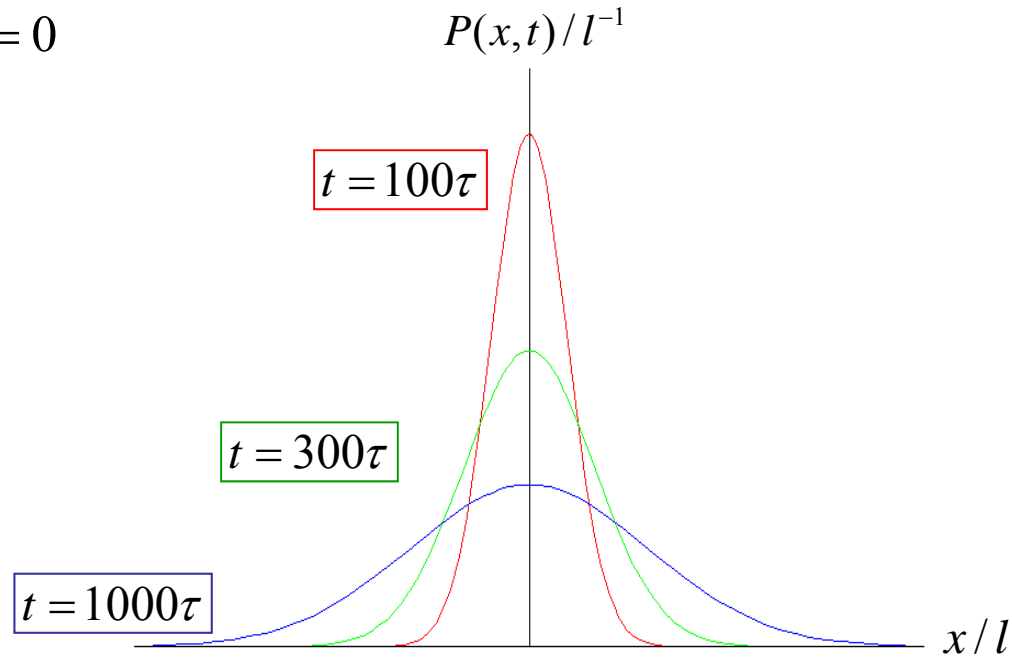
$$\frac{\partial P}{\partial t} = \left(\frac{a^2}{2\tau}\right) \frac{\partial^2 P}{\partial x^2} \quad \text{diffusion equation}$$

$D \leftarrow$

$$c(x, t) \equiv P(x, t) = \frac{1}{\sqrt{4\pi Dt}} \exp\left(-\frac{x^2}{4Dt}\right)$$

# Probability distribution of the displacements of a random walker (diffusing particle)

starting at  $x = 0$

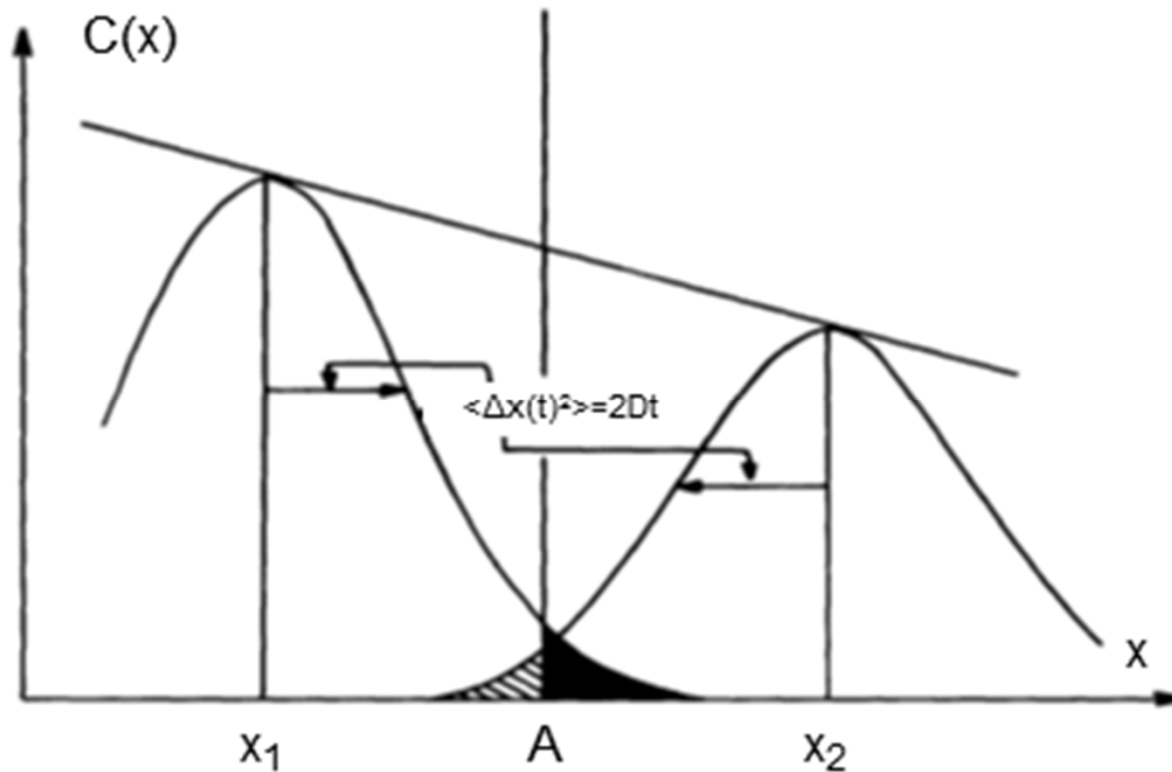


$$c(x,t) \equiv P(x,t) = \frac{1}{\sqrt{4\pi Dt}} \exp\left(-\frac{x^2}{4Dt}\right) \quad \text{(PROPAGATOR)}$$

:

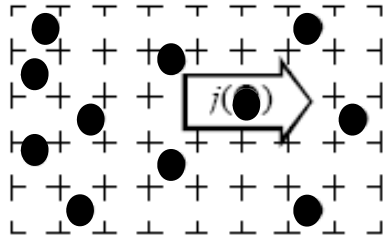


**Directed Diffusion Flux**  
generated by **Undirected Random walk**  
under the influence of a **Concentration Gradient**



# Different Situations for Recording Diffusivities

- Transport (or Collective or Chemical) Diffusion

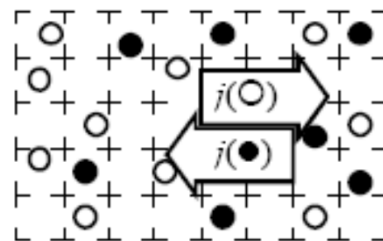


$$j_x = -D_T \frac{\partial c}{\partial x}$$

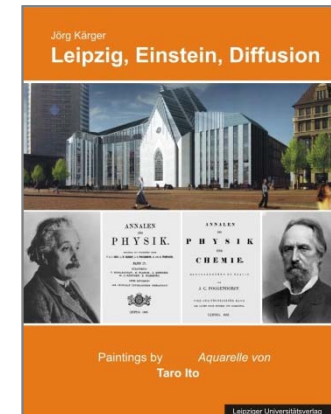
**(Fick's 1<sup>st</sup> law)**



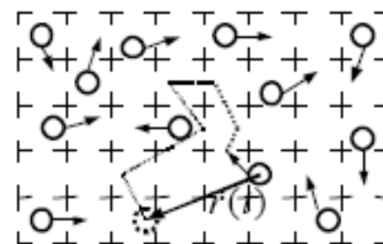
- Self- (or Tracer) Diffusion by Tracer Exchange



$$j_x^* = -D \frac{\partial c^*}{\partial x}$$

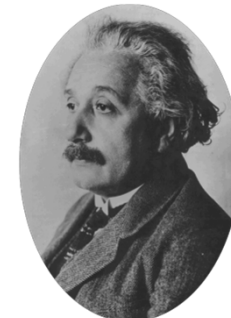


- Self- (or Tracer) Diffusion by Following the Individual Molecules

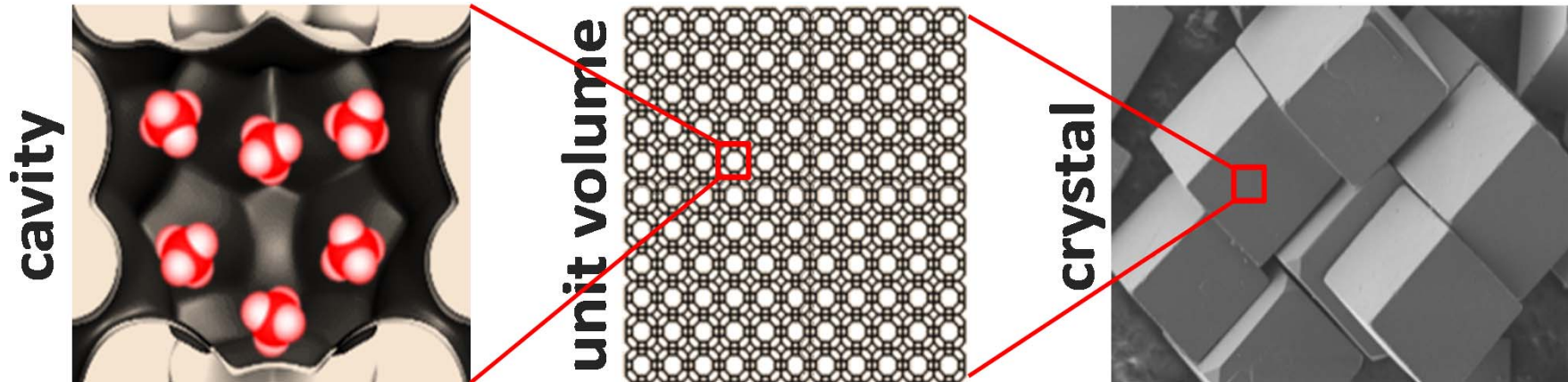


$$\langle x^2(t) \rangle = 2Dt$$

**Einstein Equation  
PFG NMR, QENS**



**Prerequisite for a meaningful definition  
of Fluxes and Concentrations  
as appearing in Fick's laws**



## **Contents:**

### **1) Tracing the diffusion path: PFG NMR diffusion measurement**

2) Recording transient concentration profiles by microimaging

3) Pore spaces „infested“ by molecules

4) Interacting invaders

5) The „driving force“ of diffusion

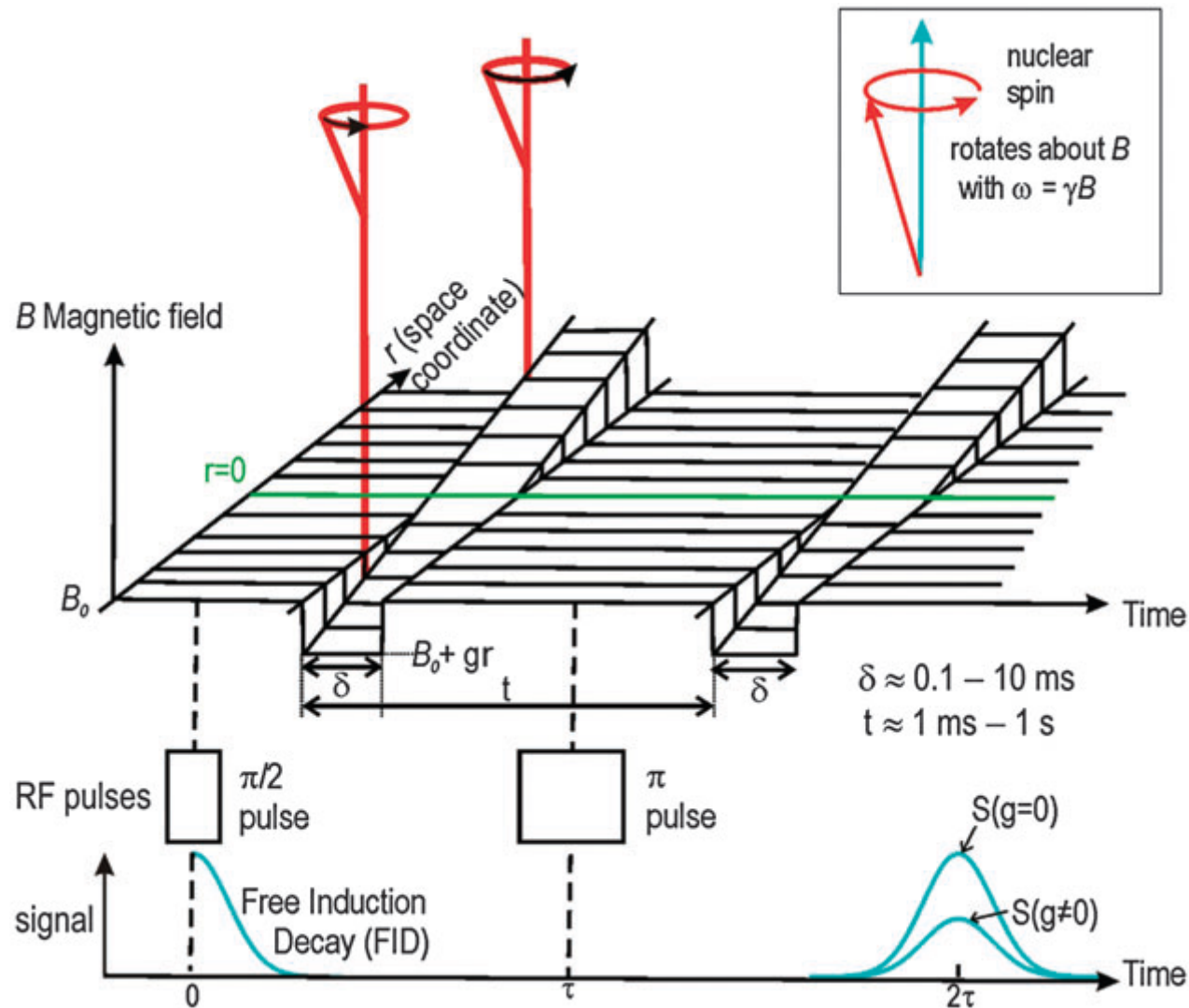
6) Transport barriers and highways

7) Spreading accompanied by guest transformation

8) Spreading accompanied by host transformation



# Diffusion Measurement by Pulsed Field Gradient (PFG) NMR



net phase  $\Delta\phi$  in rotational motion of nuclear spin

After displacement  $\Delta z$  between the two field gradient pulses:

$$\Delta\phi = \Delta(\omega\delta) = \Delta(\gamma B\delta) = \Delta[\gamma(B_0 + gz)\delta] = \gamma\delta g\Delta z$$

any spin contributes to the signal with the cosine of the phase shift  $\gamma\delta g\Delta z$ :

$$\Psi(g\delta, t) = \frac{M(g\delta, t)}{M_0(t)} = \int P(z, t) \cos(\gamma g\delta z) dz$$

With  $P(z, t)$  denoting the probability density that, during the observation time  $t$ , a molecule is shifted over a distance  $z$  (the „Propagator“)

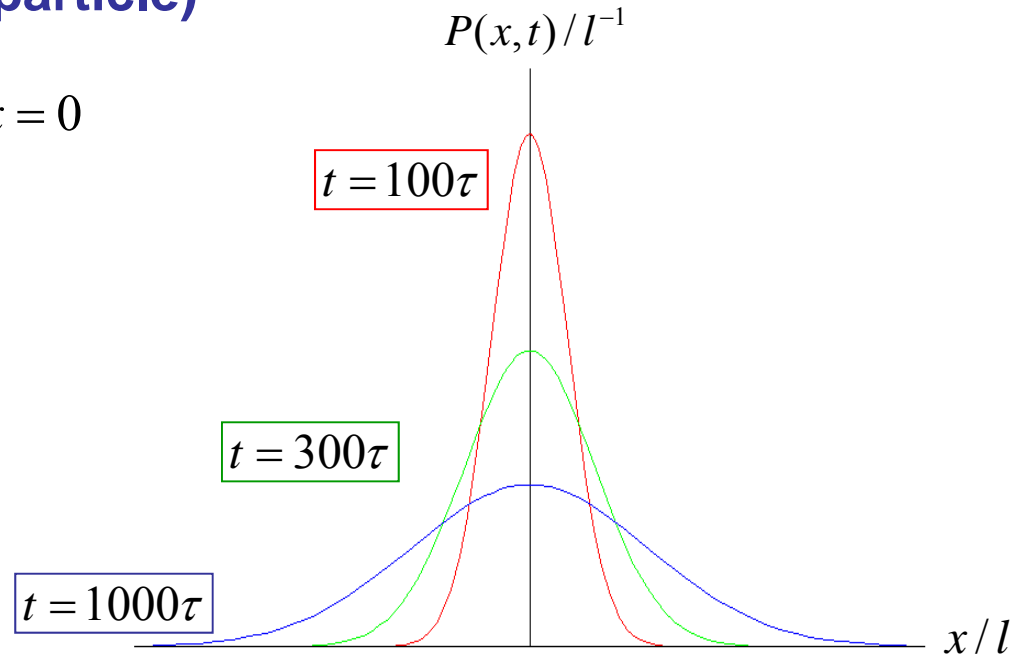
## **PFG NMR Spin-Echo Attenuation Results as the Fourier Transform of the „Propagator“**

**Vice versa: Determining the mean „Propagator“ from the Spin-Echo Attenuation:**

**J. Kärger, W. Heink: The Propagator Representation of Molecular Transport in Microporous Crystallites, J. Magn. Res. 51 (1983) 1-7**

# Probability distribution of the displacements of a random walker (diffusing particle)

starting at  $x = 0$



$$c(x,t) \equiv P(x,t) = \frac{1}{\sqrt{4\pi Dt}} \exp\left(-\frac{x^2}{4Dt}\right) \quad \textbf{(PROPAGATOR)}$$

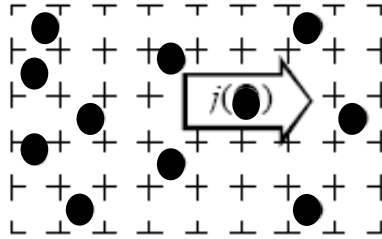
yielding the PFG NMR signal attenuation

$$\Psi(g\delta, t) = \frac{M(g\delta, t)}{M_0(t)} = \int P(z, t) \cos(\gamma g\delta z) dz$$

**Self- (or Tracer) diffusivity follows directly from the PFG NMR signal attenuation**

# The different situations in which diffusivities are measured

- Transport (or Collective or Chemical) Diffusion

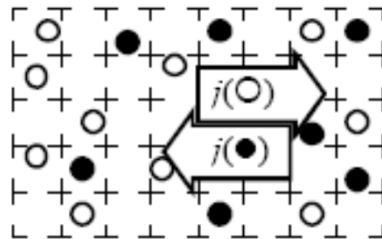


$$j_x = -D_T \frac{\partial c}{\partial x}$$

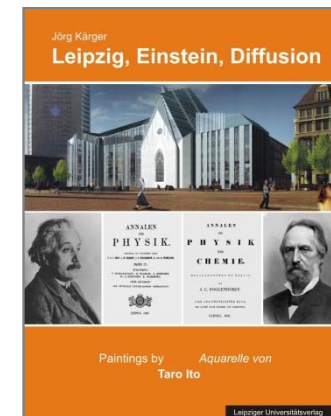
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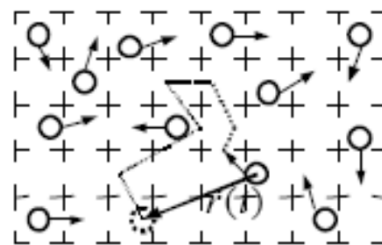
- Self-(or Tracer) Diffusion by Tracer Exchange



$$j_x^* = -D \frac{\partial c^*}{\partial x}$$



- Self- (or Tracer) Diffusion by Following the Individual Molecules (QENS, PFG NMR)



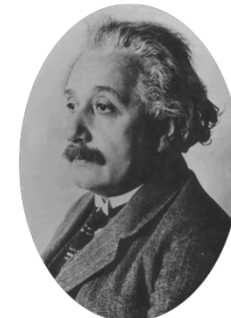
**Einstein Equation**

$$\langle x^2(t) \rangle = 2Dt$$

*Ergodic Theorem:*

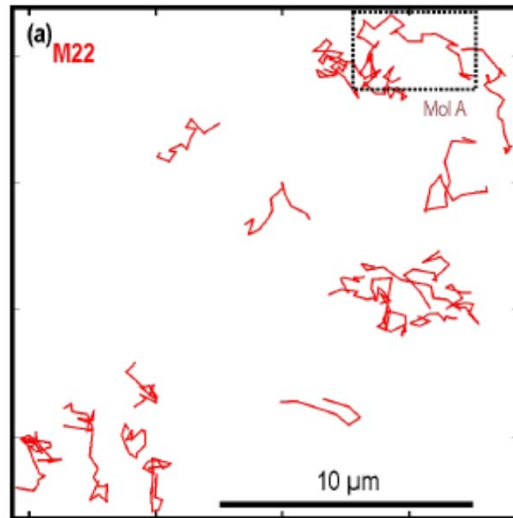
$$\langle x^2(t) \rangle_{time} = \langle x^2(t) \rangle_{ensemble}$$

?

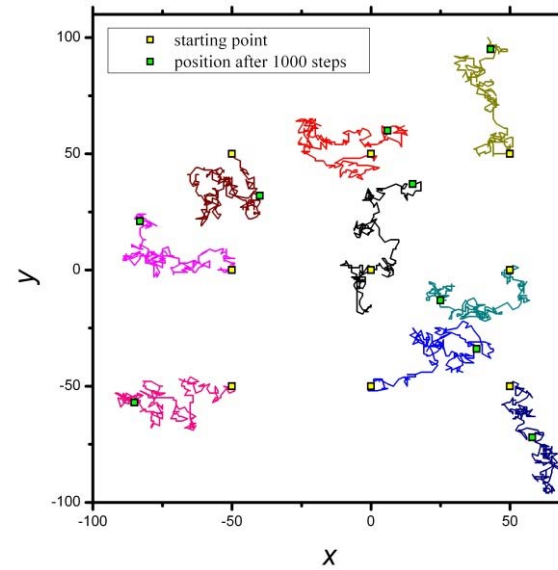




## Single-Particle Tracking by Fluorescence Microscopy

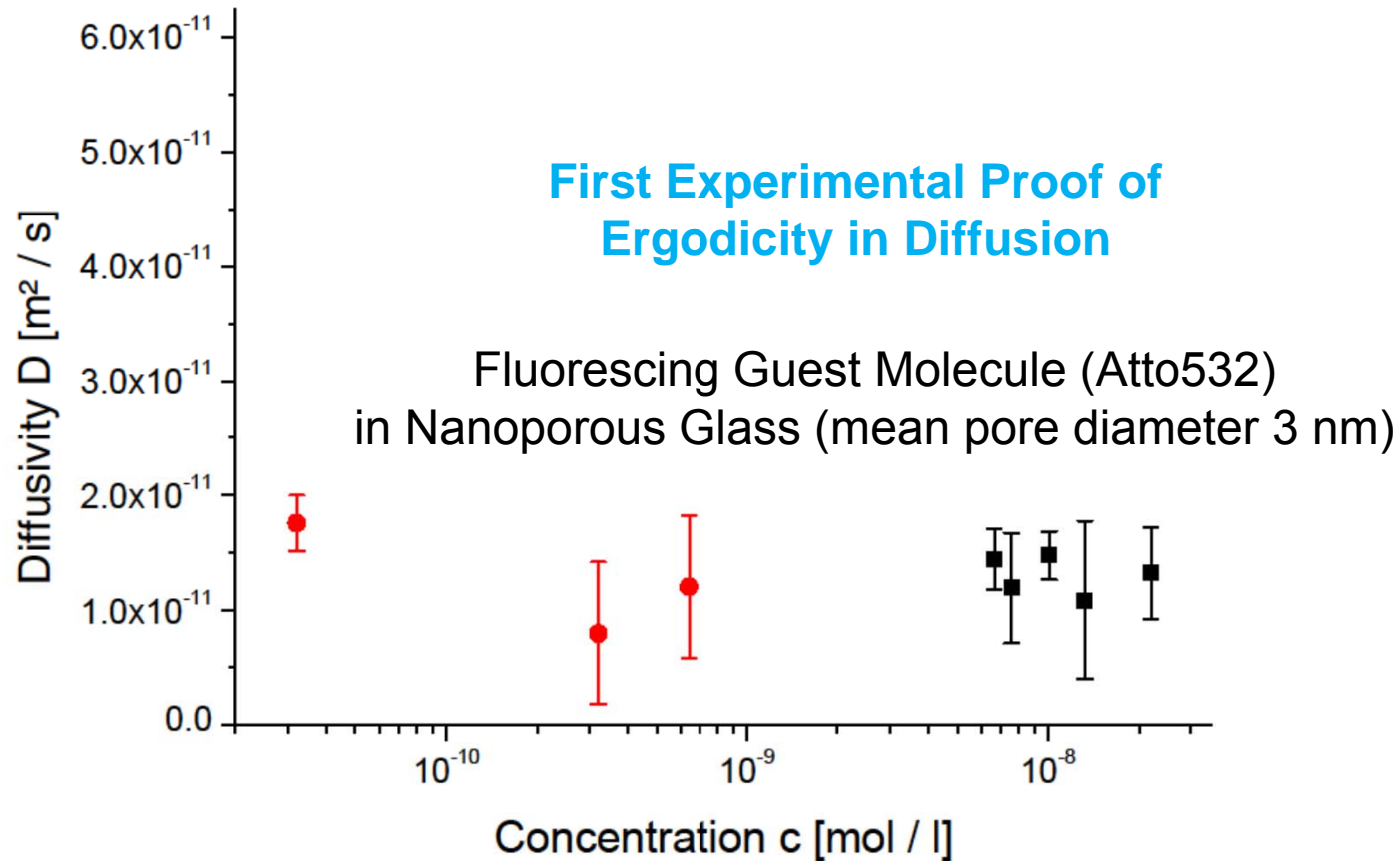


## Simulated Random Walks with Constant Step Length



## Single-Particle Time-Averaged Mean Squared Displacement

$$\langle r^2(t) \rangle_T = \frac{1}{T-t} \int_0^{T-t} [r(t'+t) - r(t')]^2 dt'$$



Single-Molecule Observation:  $D = \langle r^2(t) \rangle / 6t$

$$\langle r^2(t) \rangle_T = \frac{1}{T-t} \int_0^{T-t} [r(t'+t) - r(t')]^2 dt'$$

**Feil, F. et al: Single-Particle and Ensemble Diffusivities – Test of Ergodicity.**  
**Angew. Chem., Intern. Edit. 51 (2012) 1152**

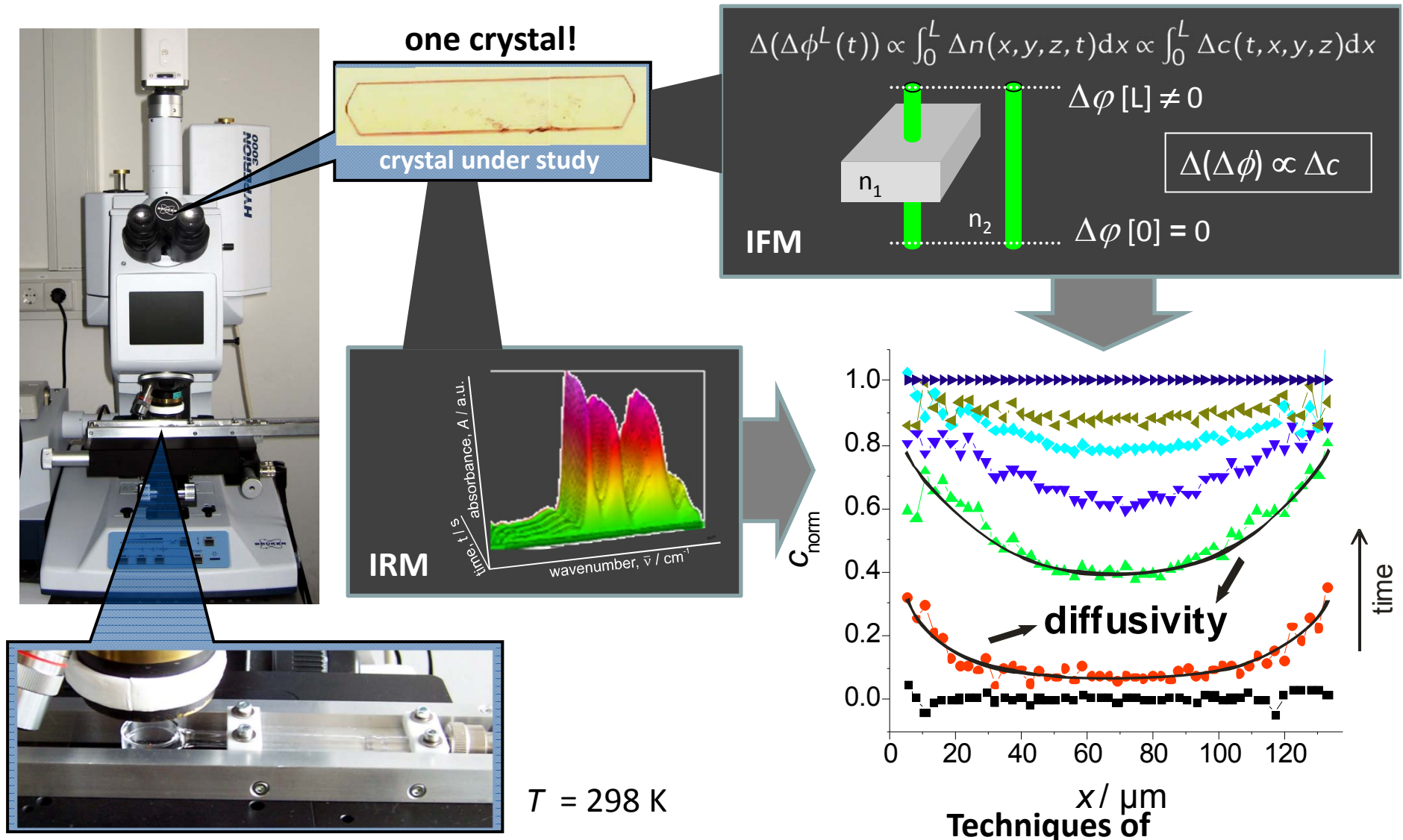
PFG NMR Measurement:

$$\langle r^2(t) \rangle_{\text{ensemble}} = \int r^2 P(r, t) dr$$

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# IR Microscopy (IRM) and Interference Microscopy (IFM)



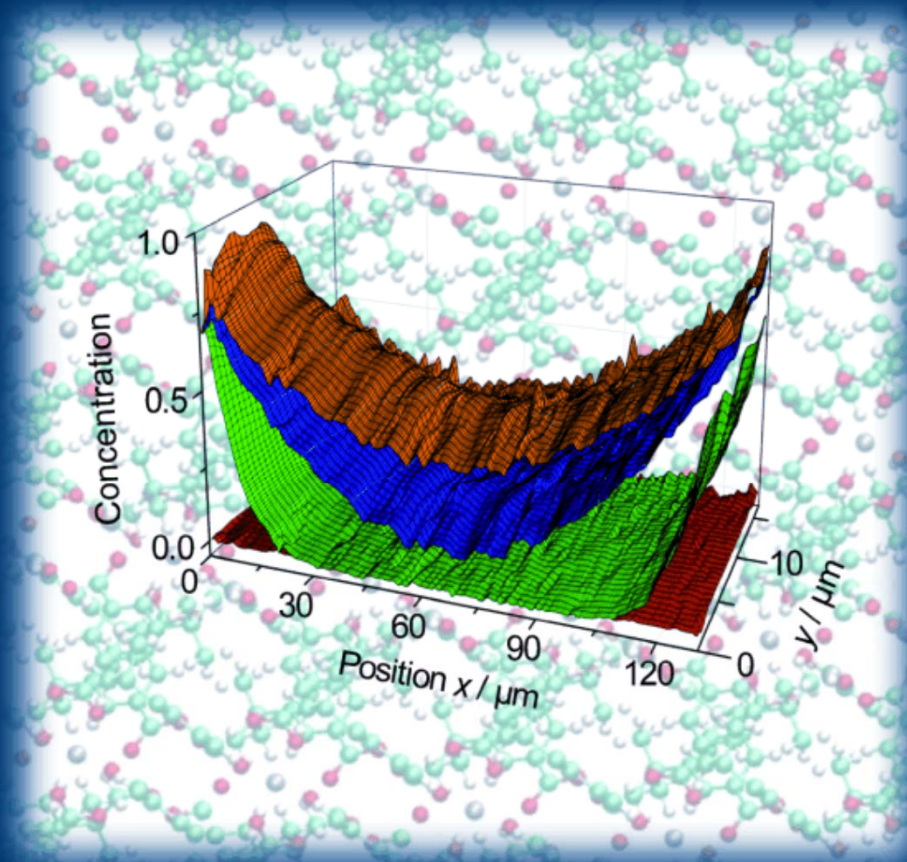
J. Kärger, T. Binder, C. Chmelik, H. Krautscheid, R. Krishna, J. Weitkamp *Nature Materials* 13 (2014) 333–343



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# CHEMPHYSICHEM

OF CHEMICAL PHYSICS AND PHYSICAL CHEMISTRY



A Journal of

15/2009



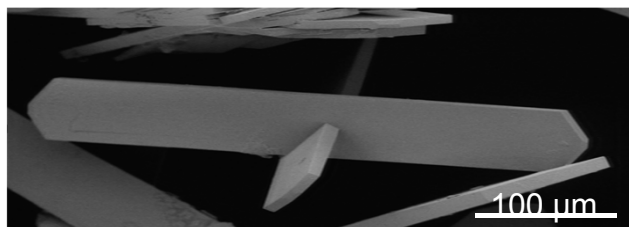
[www.chemphyschem.org](http://www.chemphyschem.org)

 WILEY-VCH

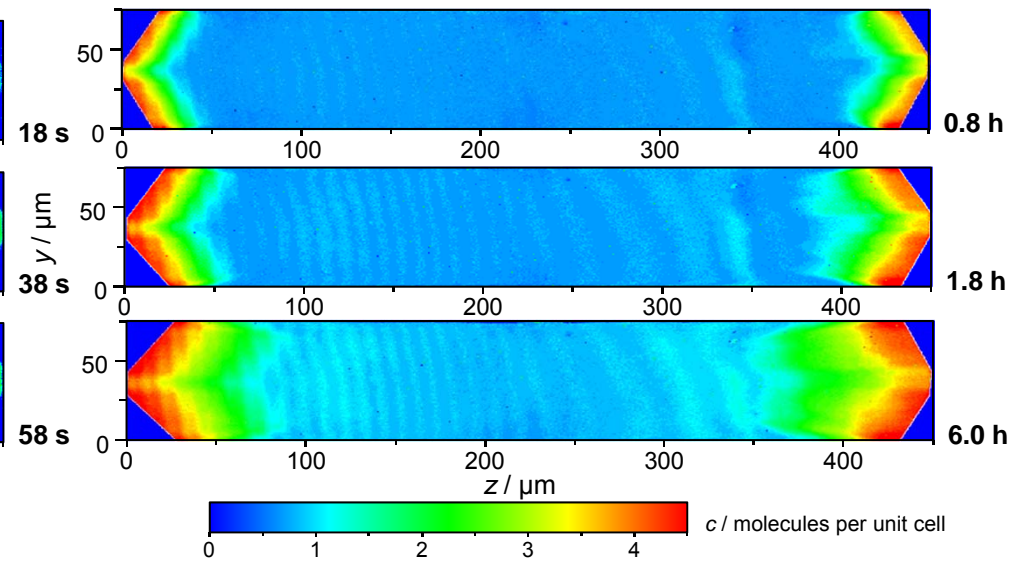
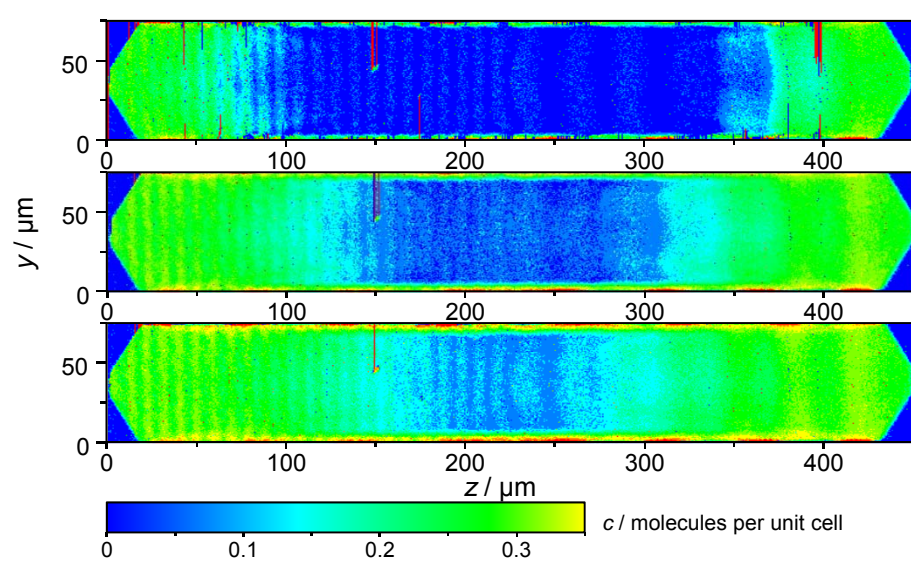
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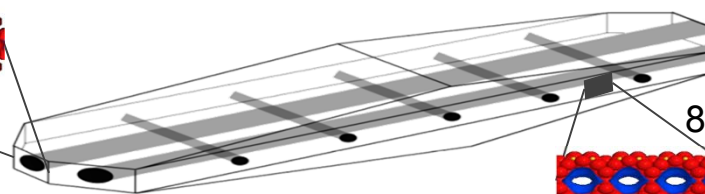
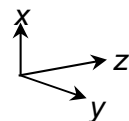
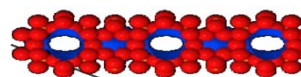
methanol adsorption,  
pressure step 0 to 0.5 kPa



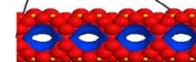
ethanol adsorption,  
pressure step 0 to 2 kPa



10-ring channels along z



8-ring channels along y

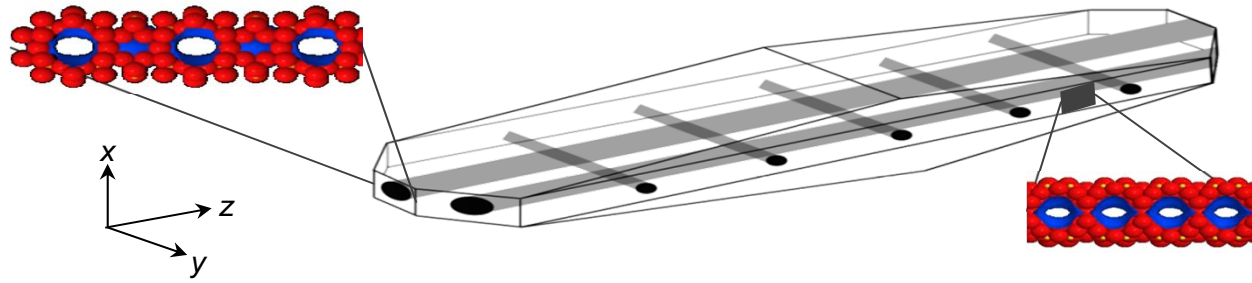


J. Kärger, T. Binder, C. Chmelik, H. Krautscheid, R. Krishna, J. Weitkamp

*Nature Materials* 13 (2014) 333–343

F. Hibbe et al: *J. Chem. Phys.* 135, 184201-1-5 (2011).

10-ring channels along z

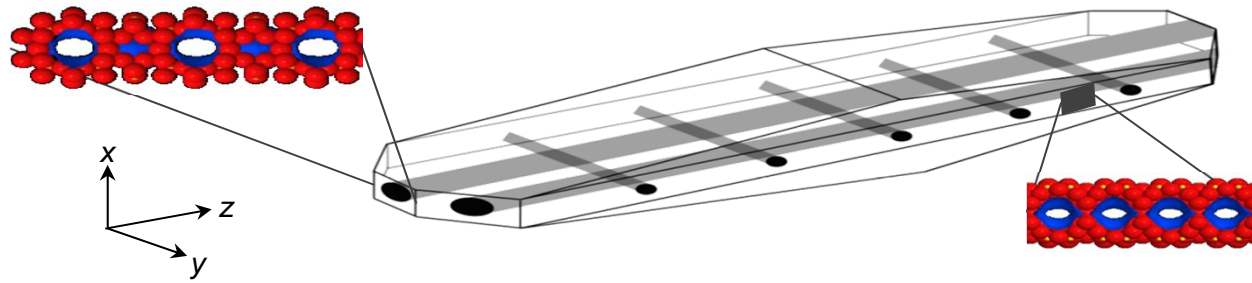


8-ring channels along y





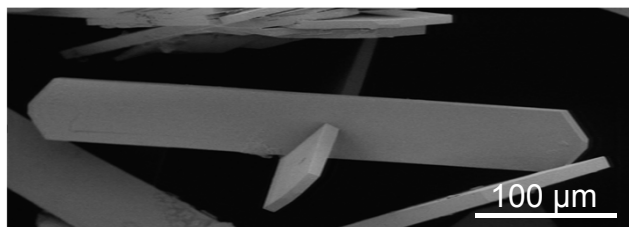
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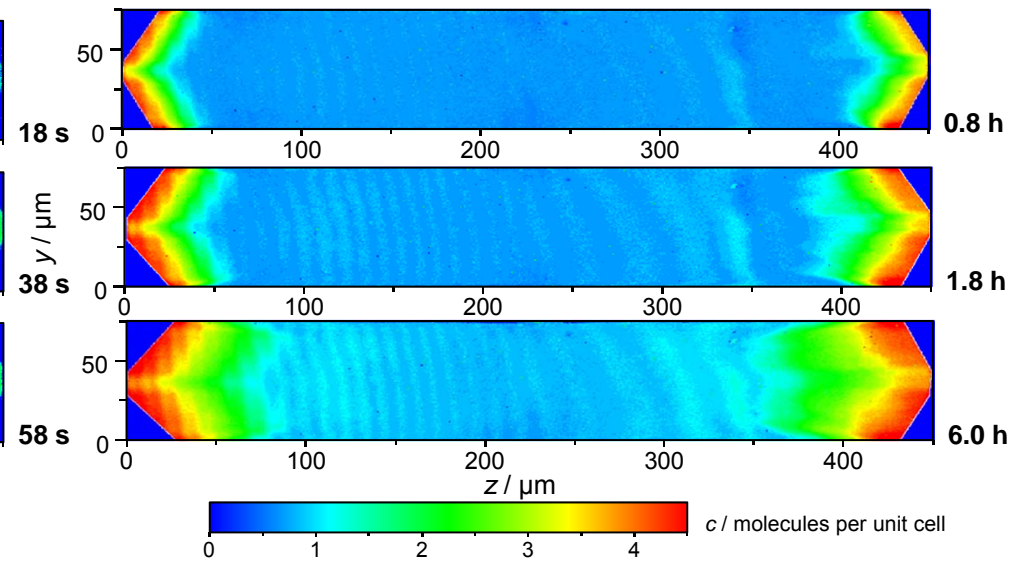
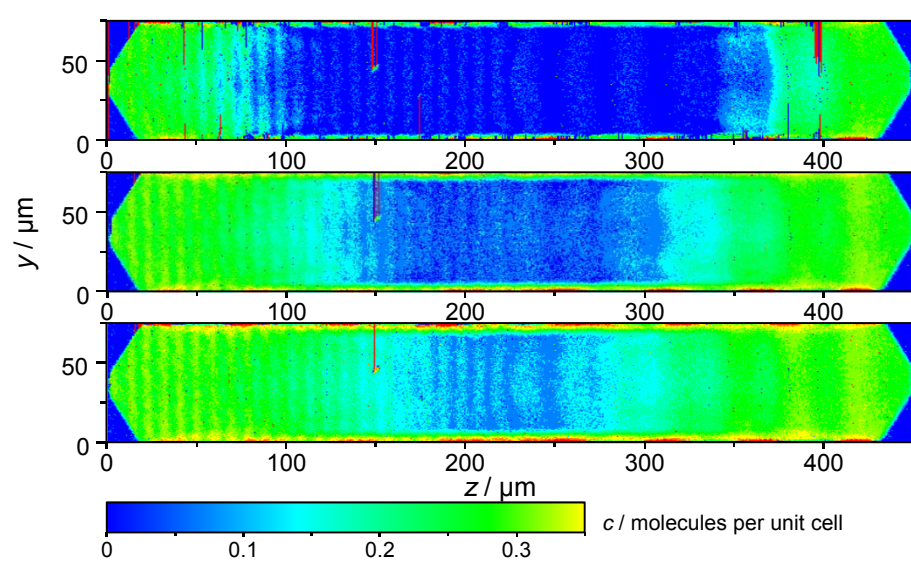
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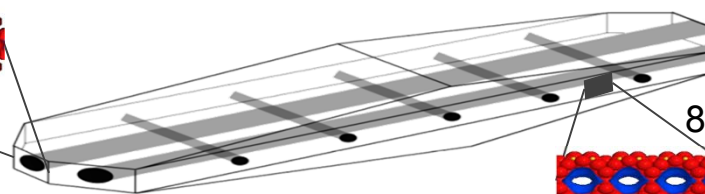
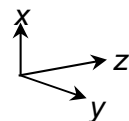
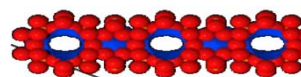
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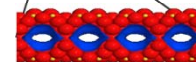
ethanol adsorption,  
pressure step 0 to 2 kPa



10-ring channels along z



8-ring channels along y



J. Kärger, T. Binder, C. Chmelik, H. Krautscheid, R. Krishna, J. Weitkamp

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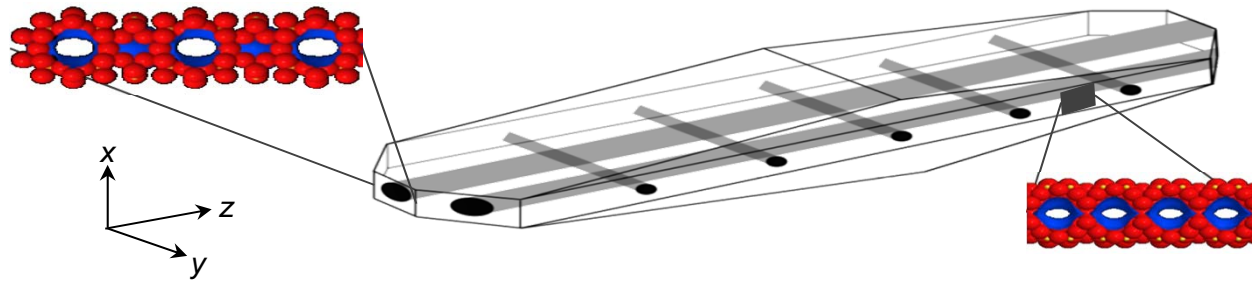
F. Hibbe et al: *J. Chem. Phys.* 135, 184201-1-5 (2011)



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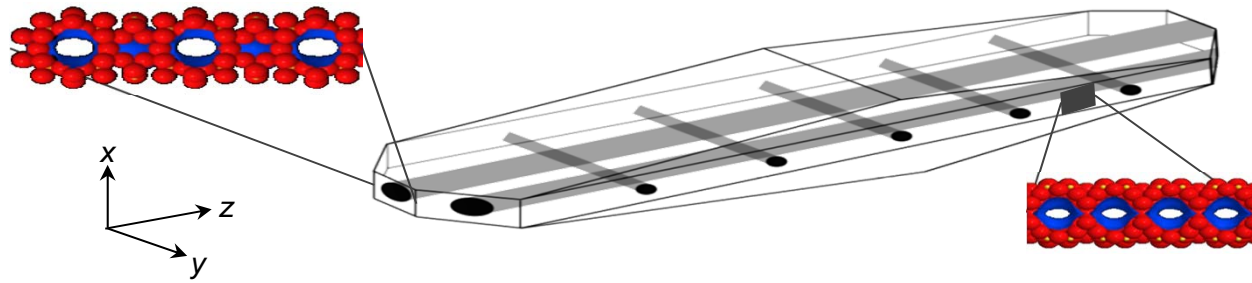
10-ring channels along z



8-ring channels along y



10-ring channels along z

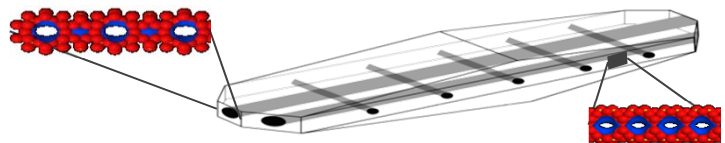


8-ring channels along y



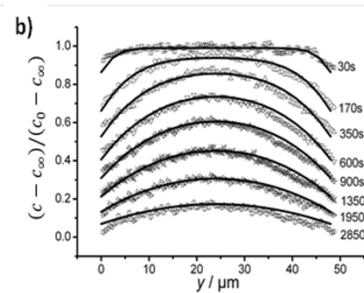
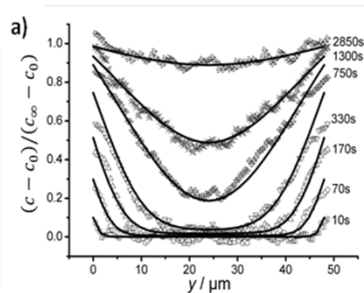
# Uptake and Release of methanol along the 8-ring channels of Zeolite Ferrierite:

10-ring channels along z sealed



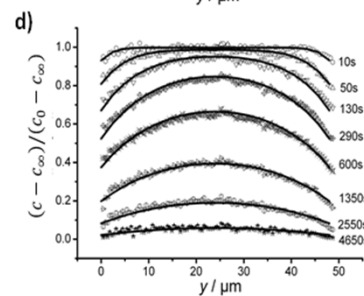
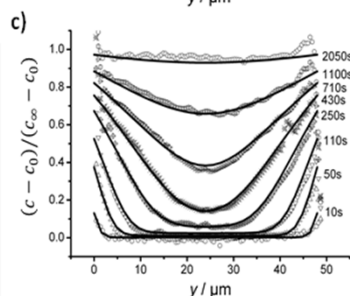
8-ring channels along y

0 to 5 mbar



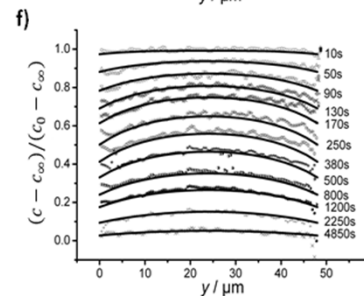
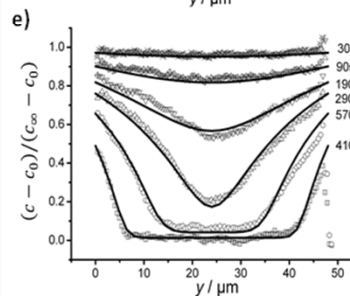
5 to 0 mbar

0 to 10 mbar



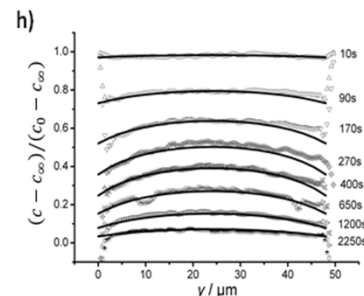
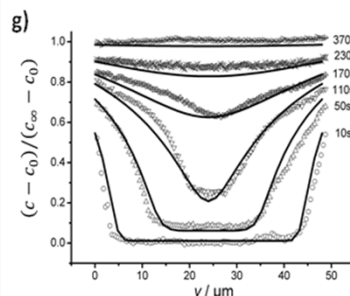
10 to 0 mbar

0 to 40 mbar



40 to 0 mbar

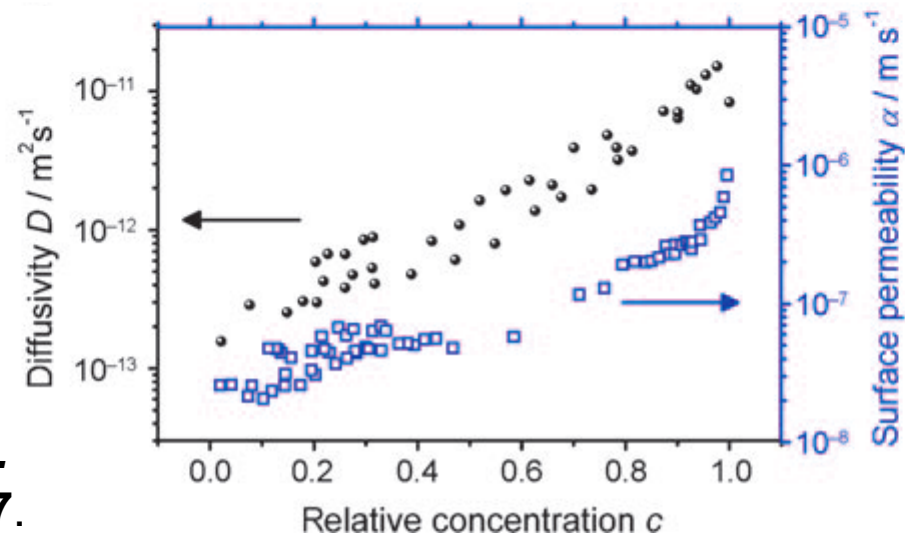
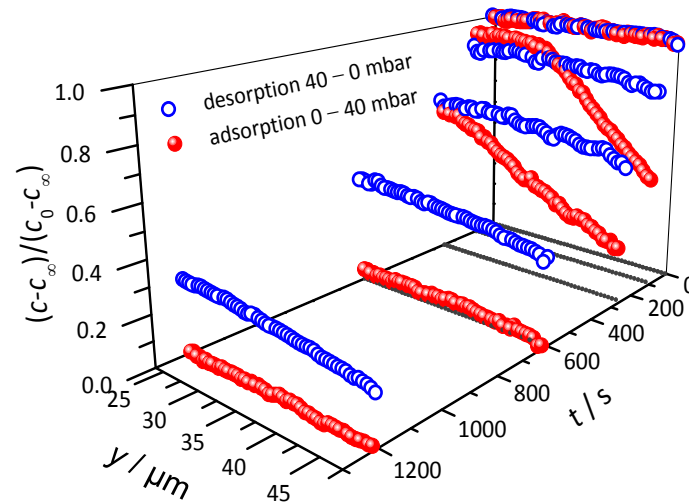
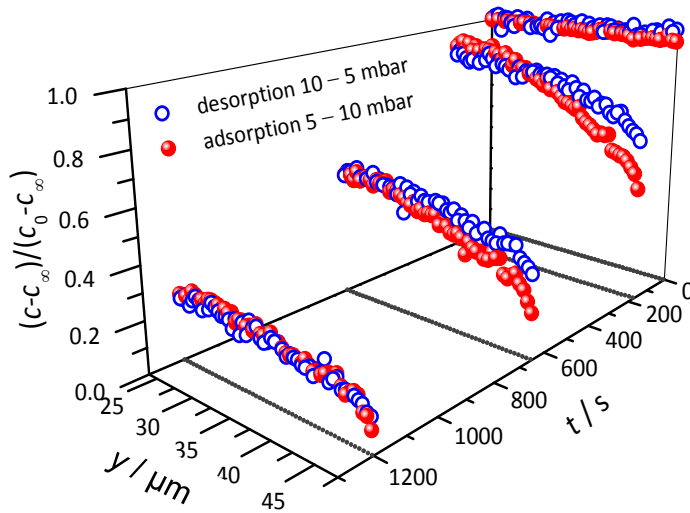
0 to 80 mbar



80 to 0 mbar



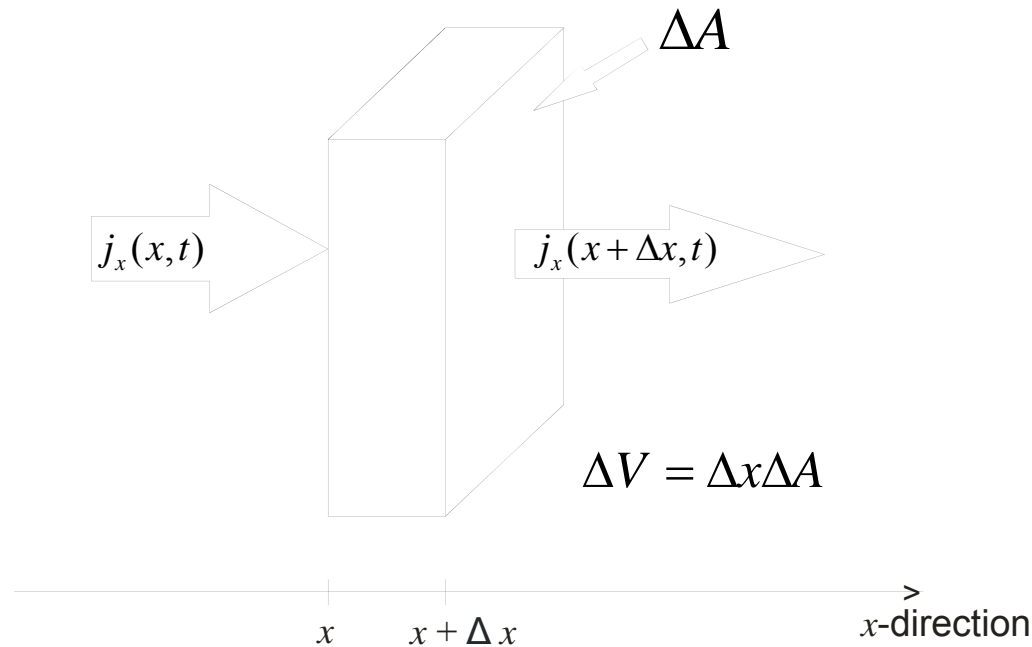
## Uptake (**Adsorption**) and Release (**Desorption**) of methanol along the 8-ring channels of Zeolite Ferrierite



$$j = \alpha (c_{\text{boundary}} - c_{\text{equilibrium}})$$

**C. Chmelik et al.**  
**Chem. Phys. Chem.**  
**2009, 10, 2623–2627.**

## From Fluxes to Concentration Changes



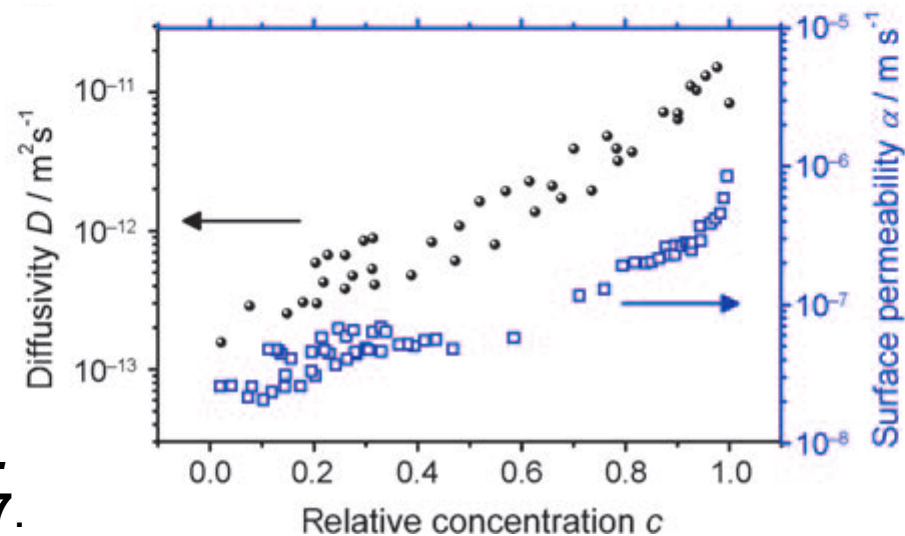
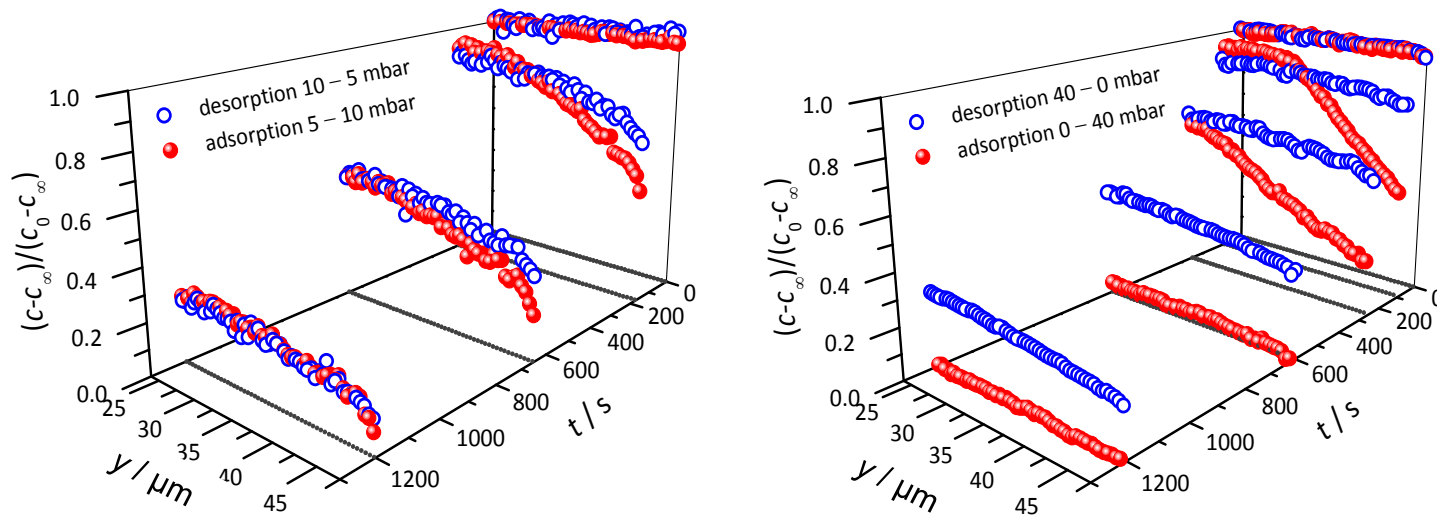
$$\frac{\partial c}{\partial t} \equiv \frac{1}{\Delta V} \frac{\partial N}{\partial t} \approx \frac{1}{\Delta V} \frac{\Delta N}{\Delta t} = \frac{1}{\Delta A \Delta x} \frac{(j_x(x) - j_x(x + \Delta x)) \Delta A \Delta t}{\Delta t} = \frac{j_x(x) - j_x(x + \Delta x)}{\Delta x} \approx -\frac{\partial j}{\partial x}$$

Inserting Fick's 1<sup>st</sup> law  $j = -D \frac{\partial c}{\partial x}$  yields

$$\begin{aligned} \frac{\partial c}{\partial t} &= \frac{\partial}{\partial x} \left( D \frac{\partial c}{\partial x} \right) = D \frac{\partial^2 c}{\partial x^2} + \frac{\partial D}{\partial x} \frac{\partial c}{\partial x} = D \frac{\partial^2 c}{\partial x^2} + \frac{\partial D}{\partial c} \left( \frac{\partial c}{\partial x} \right)^2 \\ &= D \frac{\partial^2 c}{\partial x^2} \quad (\text{for constant diffusivities}) \end{aligned} \quad \boxed{\text{(Fick's 2<sup>nd</sup> law)}}$$



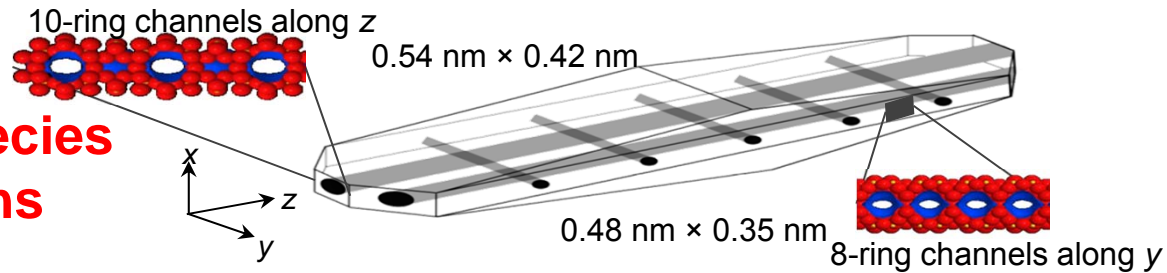
## Uptake (**Adsorption**) and Release (**Desorption**) of methanol along the 8-ring channels of Zeolite Ferrierite



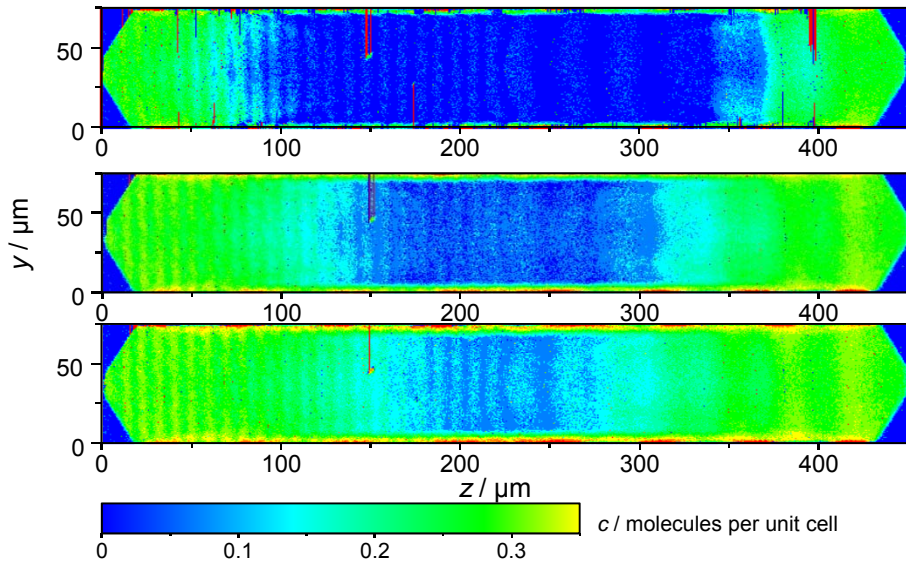
$$j = \alpha (c_{\text{boundary}} - c_{\text{equilibrium}})$$

**C. Chmelik et al.**  
**Chem. Phys. Chem.**  
**2009, 10, 2623–2627.**

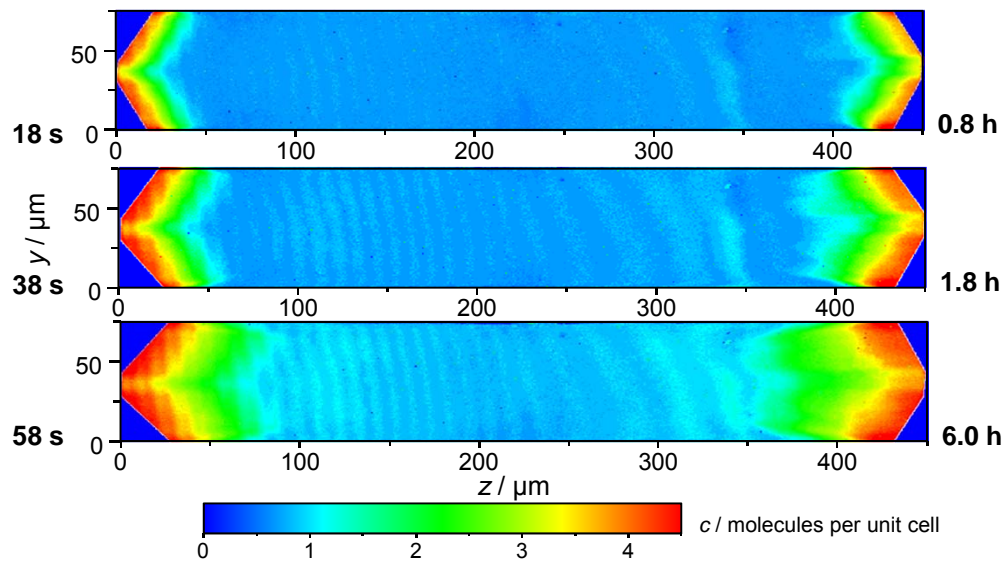
# Infestation by Second Species Changes Diffusion Paths



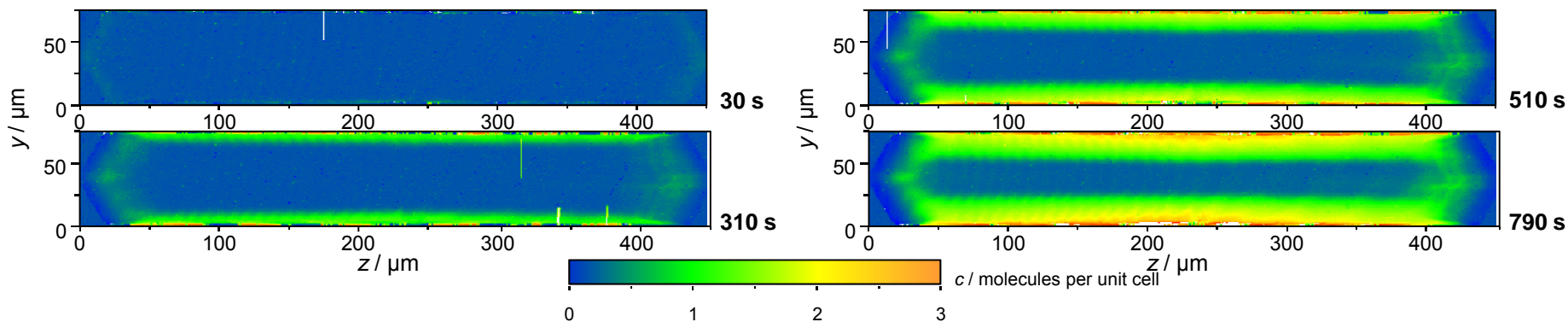
**methanol adsorption, pressure step 0 to 0.5 kPa**



**ethanol adsorption, pressure step 0 to 2 kPa**

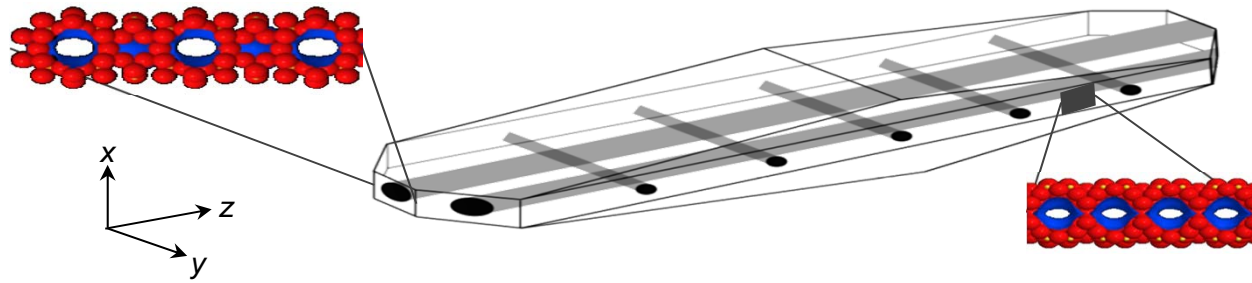


**methanol adsorption (pressure step 0 to 4 kPa) after 1.8 h ethanol pre-adsorption (pressure step 0 to 2 kPa)**



**J. Kärger, T. Binder, C. Chmelik, H. Krautscheid, R. Krishna, J. Weitkamp**  
*Nature Materials* 13 (2014) 333–343

10-ring channels along z

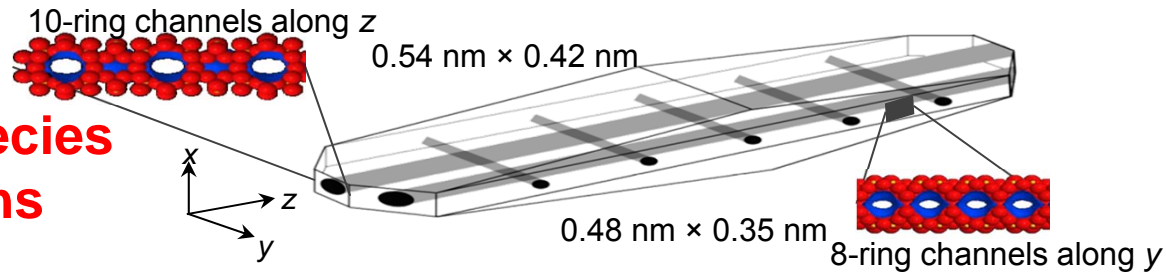


8-ring channels along y

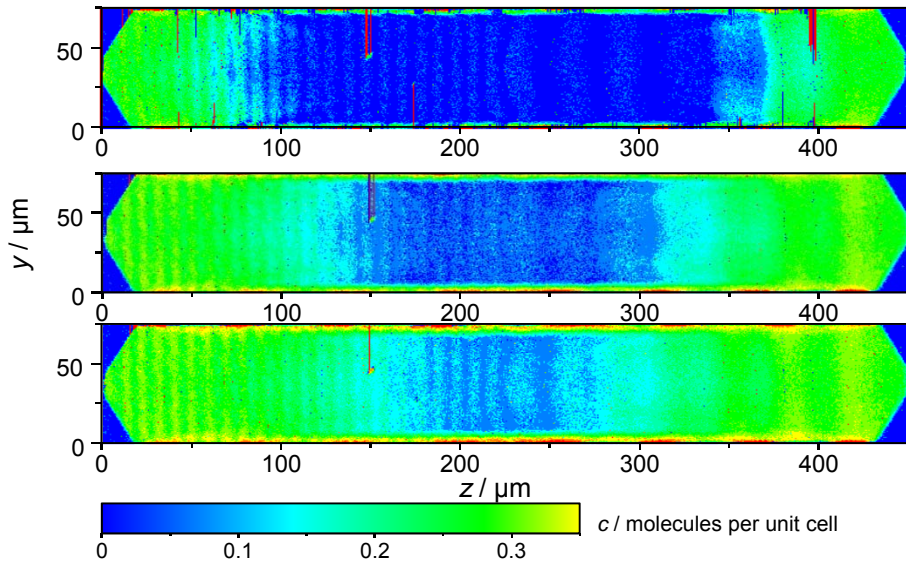




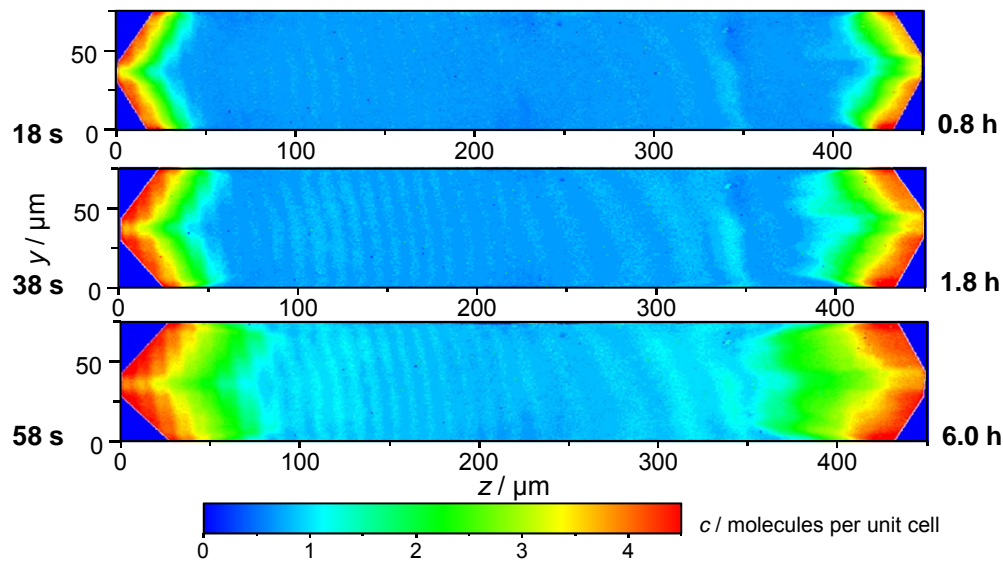
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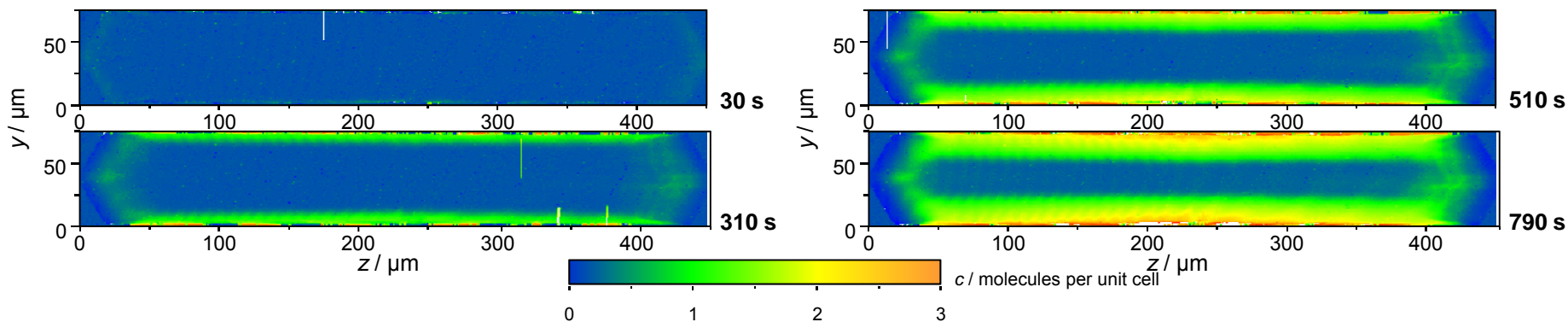
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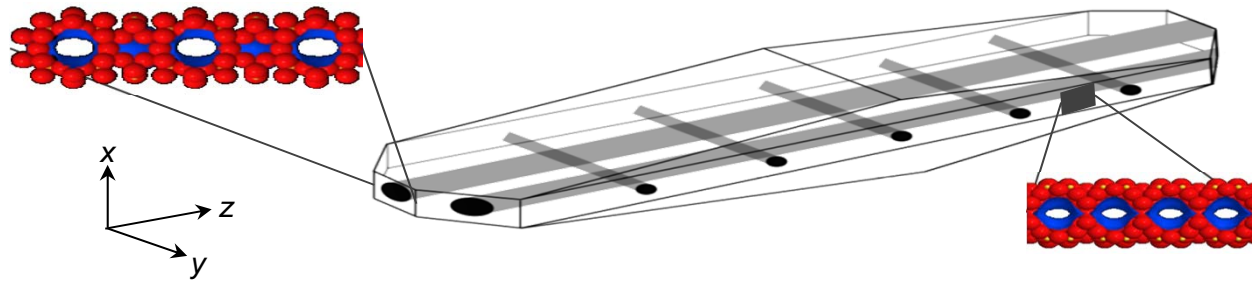


methanol adsorption (pressure step 0 to 4 kPa) after 1.8 h ethanol pre-adsorption (pressure step 0 to 2 kPa)



**J. Kärger, T. Binder, C. Chmelik, H. Krautscheid, R. Krishna, J. Weitkamp**  
*Nature Materials* 13 (2014) 333–343

10-ring channels along z

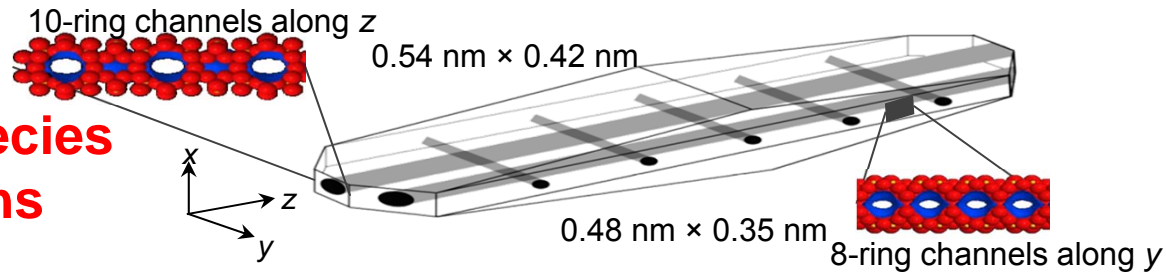


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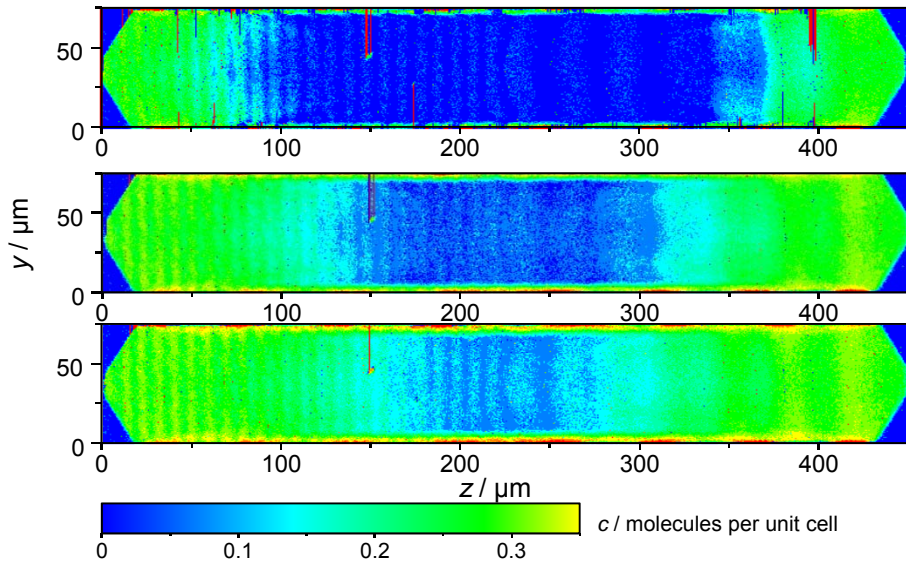




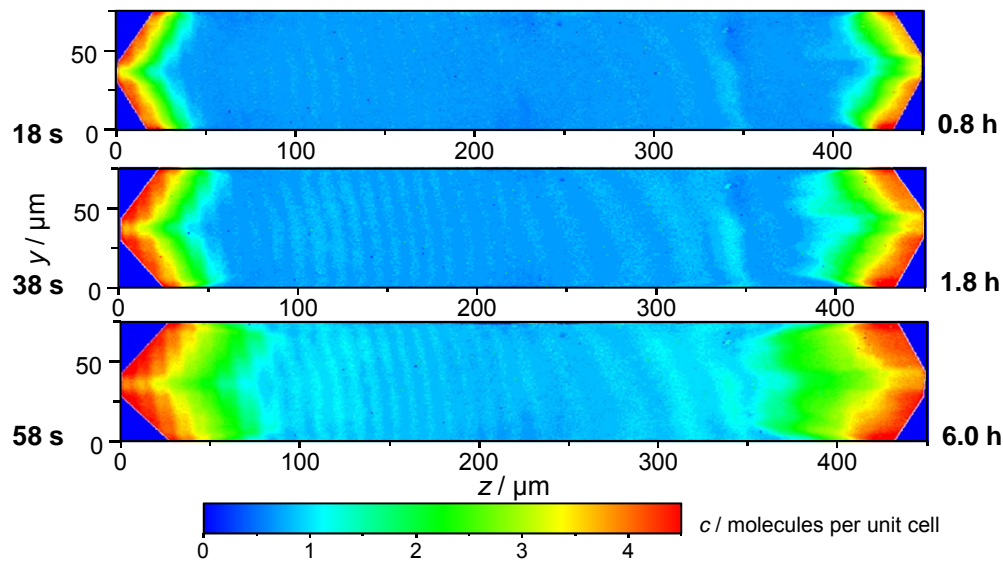
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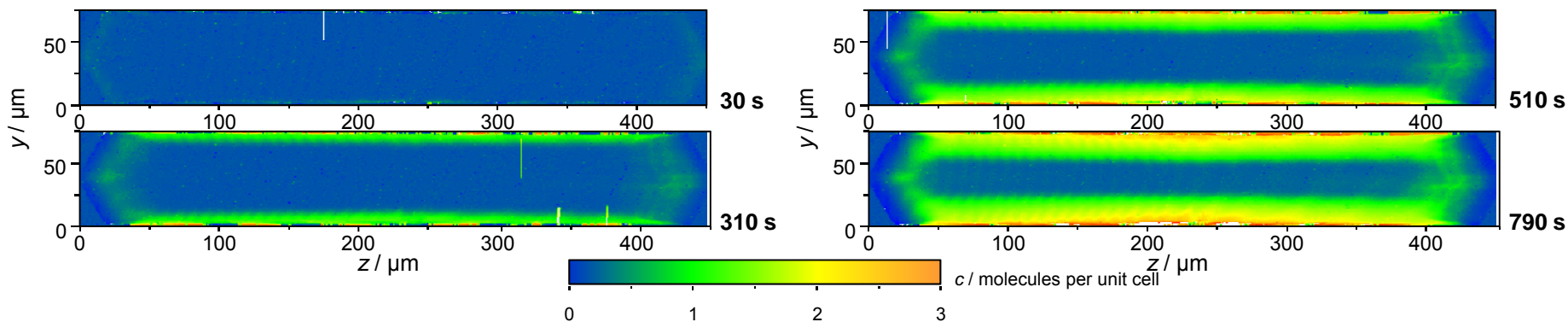
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*Nature Materials* 13 (2014) 333–343

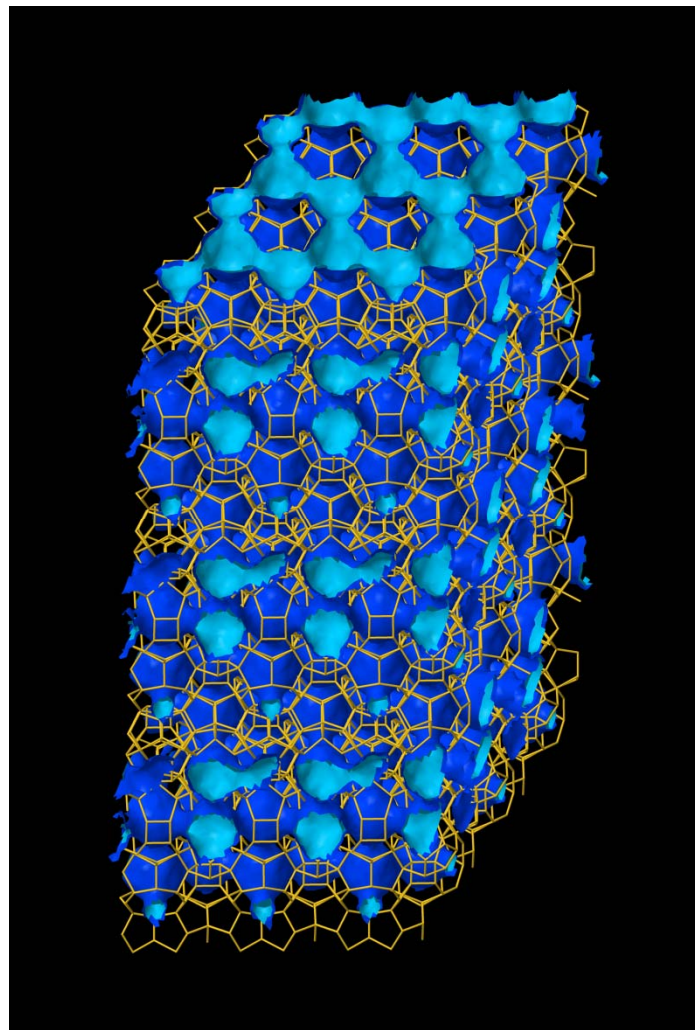
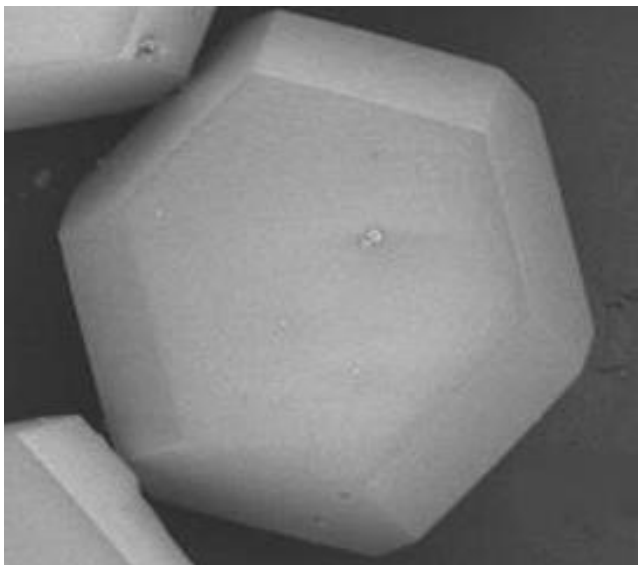
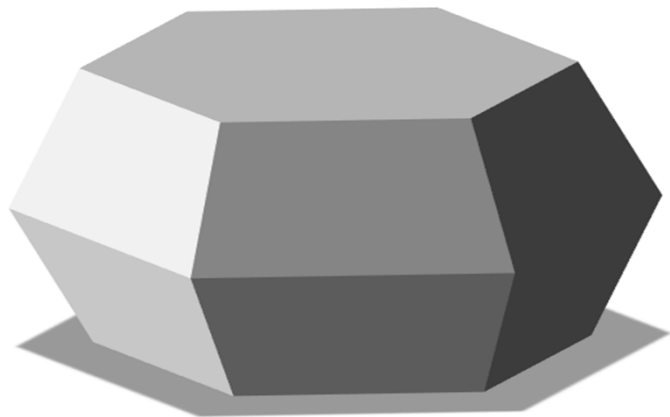


## **Contents:**

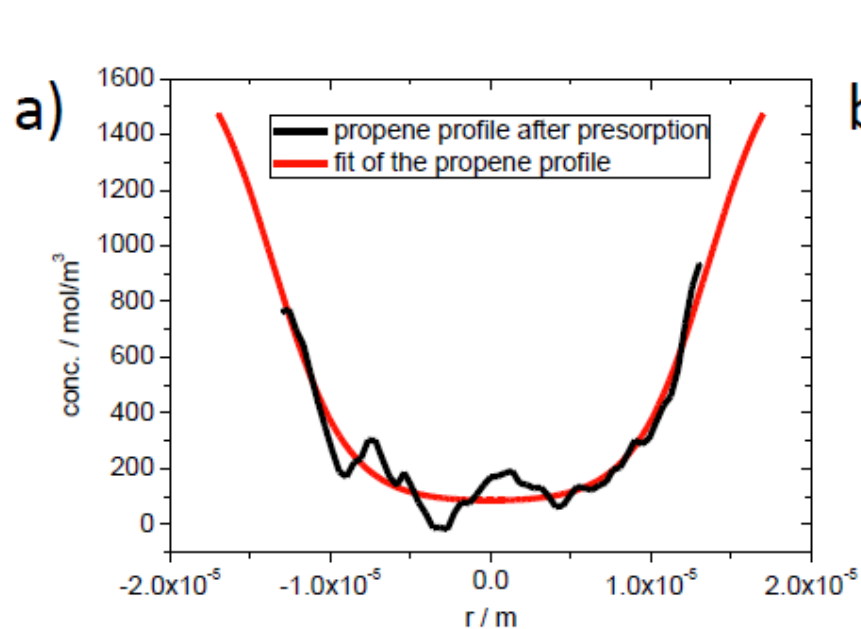
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- 5) The „driving force“ of diffusion**
- 6) Transport barriers and highways
- 7) Spreading accompanied by guest transformation
- 8) Spreading accompanied by host transformation

# Diffusion uphill?

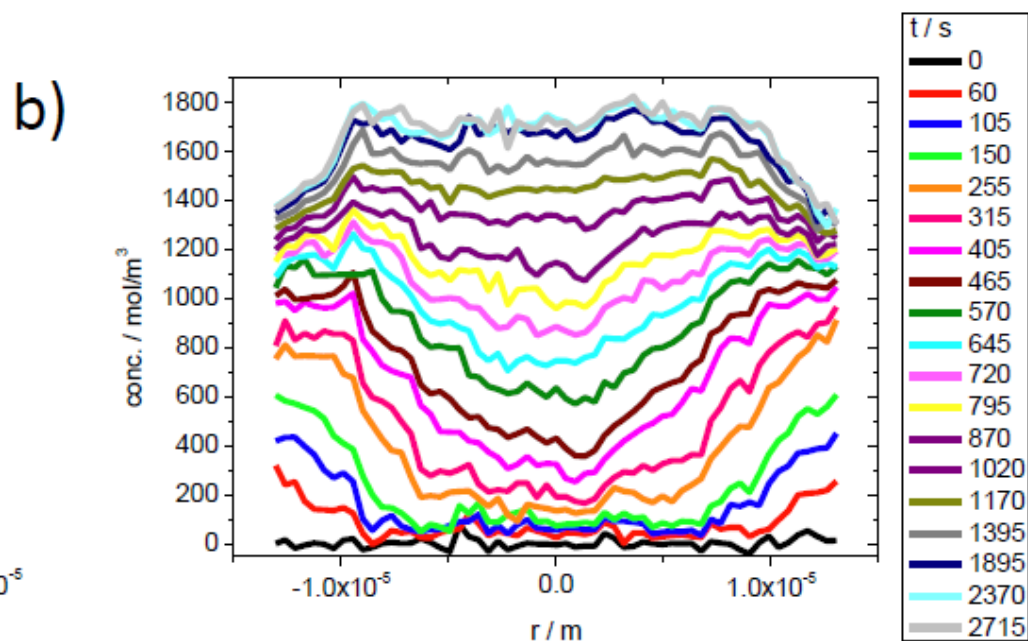
Our Working Horse: **Zeolite ZSM-58 (Structure Type DDR)**



# Evolution of Ethane Concentration in DDR after Propene Pre-Adsorption



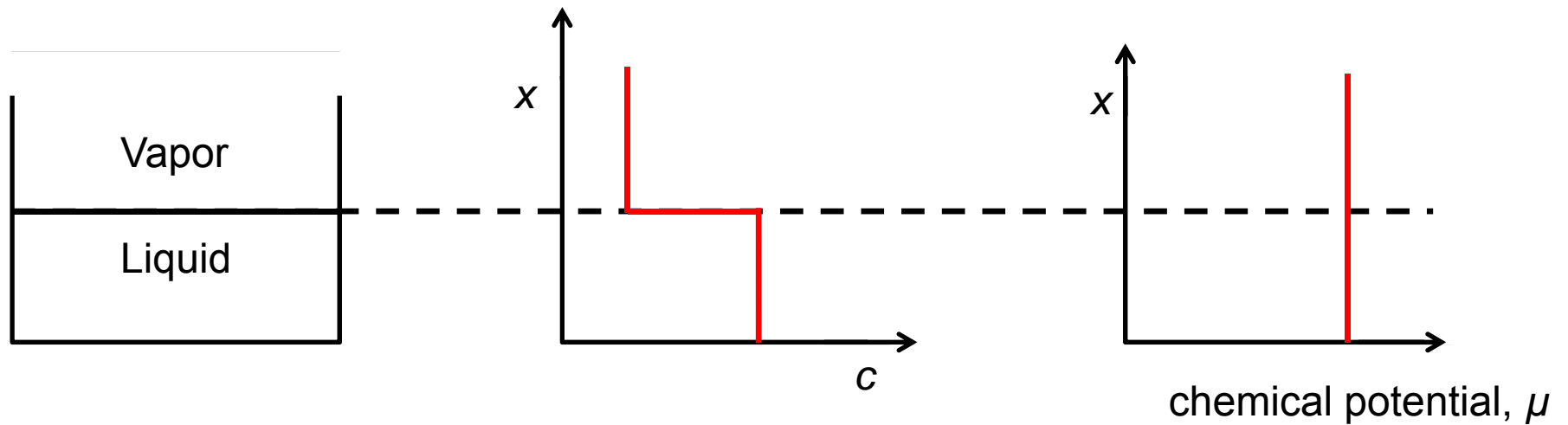
**Propene Concentration in DDR**  
after 7 hours in propene atmosphere



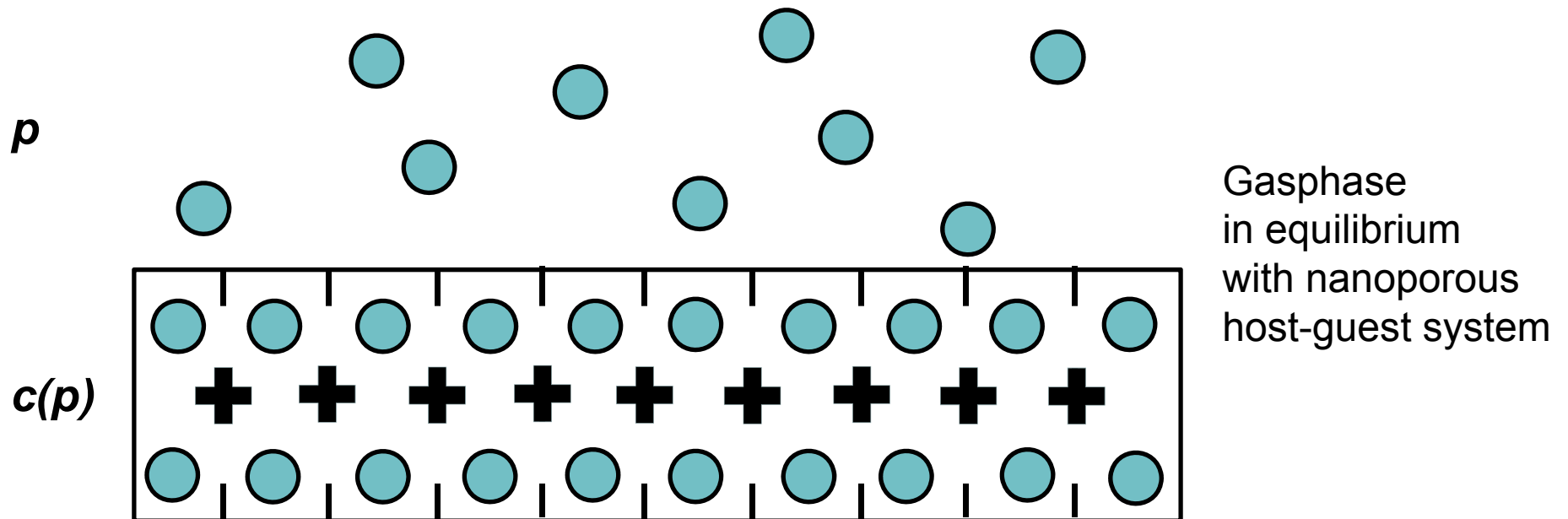
**Evolution of Ethane Profile in DDR**  
under the influence of pre-adsorbed propene

A. Lauerer, T. Binder, C. Chmelik, E. Miersemann, J. Haase, D. M. Ruthven, J. Kärger, Nature Communications 6, 7697 (2015).

# Driving Force of Diffusion



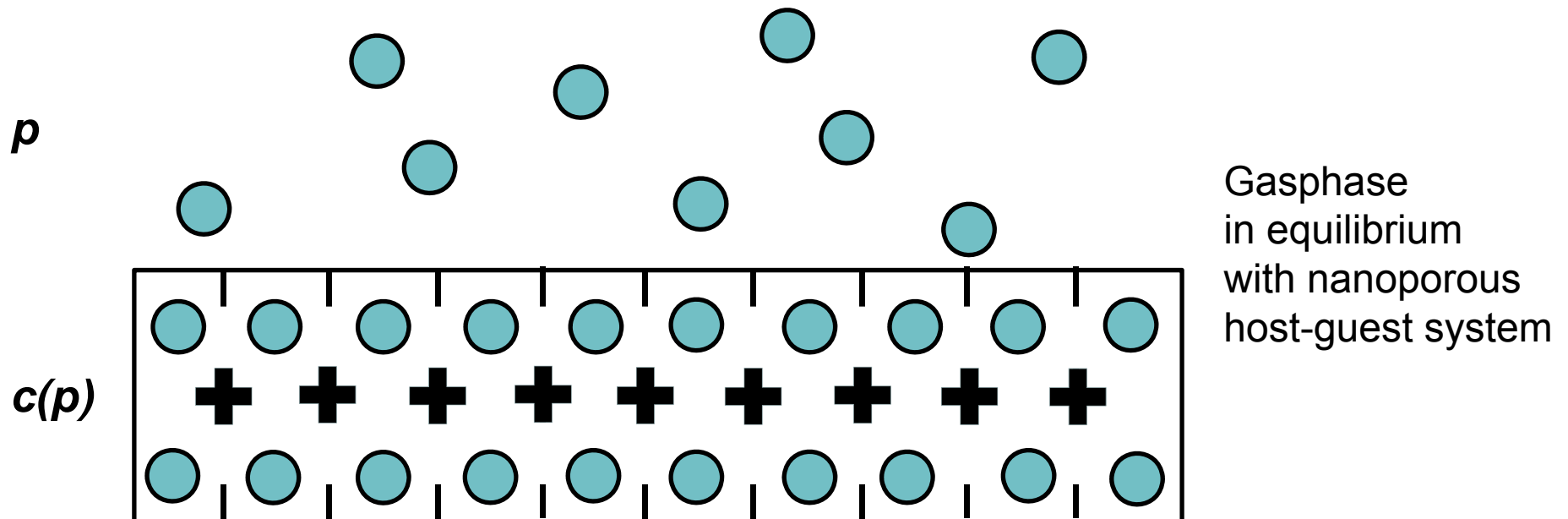
$$\mu = RT \ln p_{equilibrium}$$



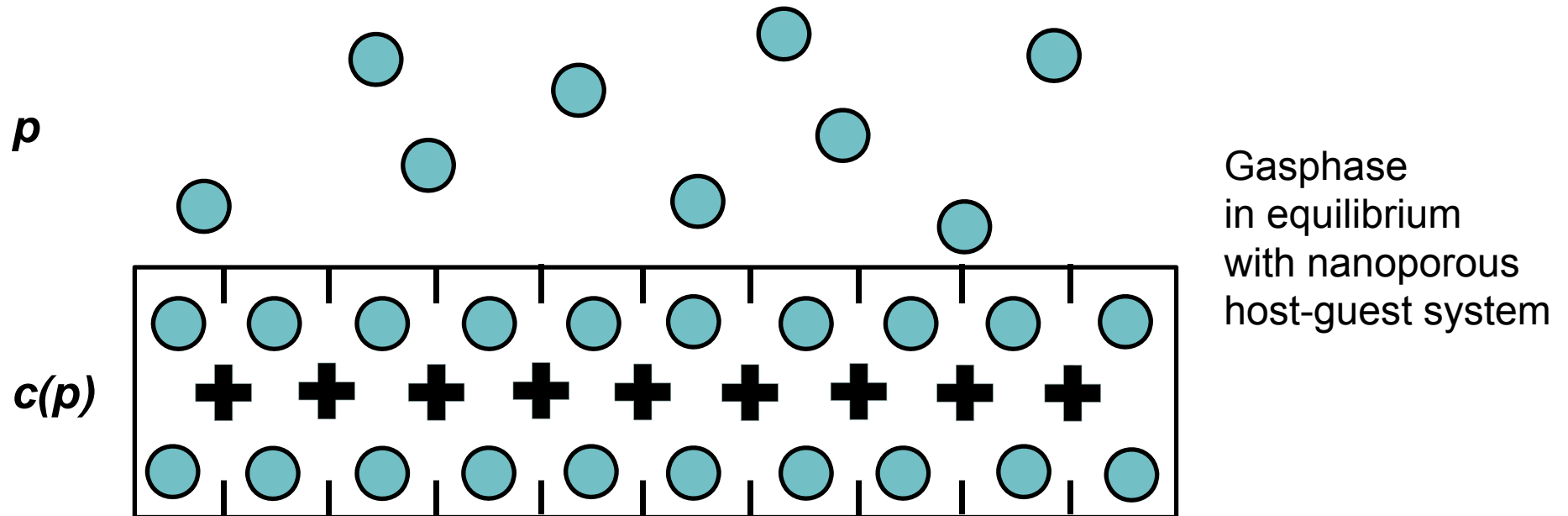
# Driving Force of Diffusion

$$\mu = RT \ln p_{equilibrium}$$

Correlations between chemical potential and guest pressure are here and in the following explicitly mentioned only for completeness:  
All relevant features of mass transfer are accessible by simply considering the respective equilibrium gas pressure



# Driving Force of Diffusion



Single-component host-guest system

$$j \propto c \frac{\partial \mu}{\partial x} \propto c \frac{\partial \ln p}{\partial x} \propto c \frac{\partial \ln p(c)}{\partial c} \frac{\partial c}{\partial x} = \frac{\partial \ln p(c)}{\partial \ln c} \frac{\partial c}{\partial x}$$

yields Fick's 1st law

$$j = \text{concentration dependent factor} \times \frac{\partial c}{\partial x}$$

Different Situation with two Components:  
 Equilibrium pressure and hence the chemical potential  
 is now a function of both components:

$$p_{ethane} = p(c_{ethane}, c_{propene})$$

Instead of the procedure just considered for one-component guests

$$j \propto c \frac{\partial \mu}{\partial x} \propto c \frac{\partial \ln p}{\partial x} \propto c \frac{\partial \ln p(c)}{\partial c} \frac{\partial c}{\partial x} = \frac{\partial \ln p(c)}{\partial \ln c} \frac{\partial c}{\partial x}$$

The presence of two guest components (1,2) must be considered:

$$j_{ethane(1)} \propto c_1 \frac{\partial \mu_1}{\partial x} \propto c_1 \left[ \frac{\partial \ln p(c_1, c_2)}{\partial c_1} \frac{\partial c_1}{\partial x} + \frac{\partial \ln p(c_1, c_2)}{\partial c_2} \frac{\partial c_2}{\partial x} \right]$$

Flux is seen to depend on both concentration gradients:

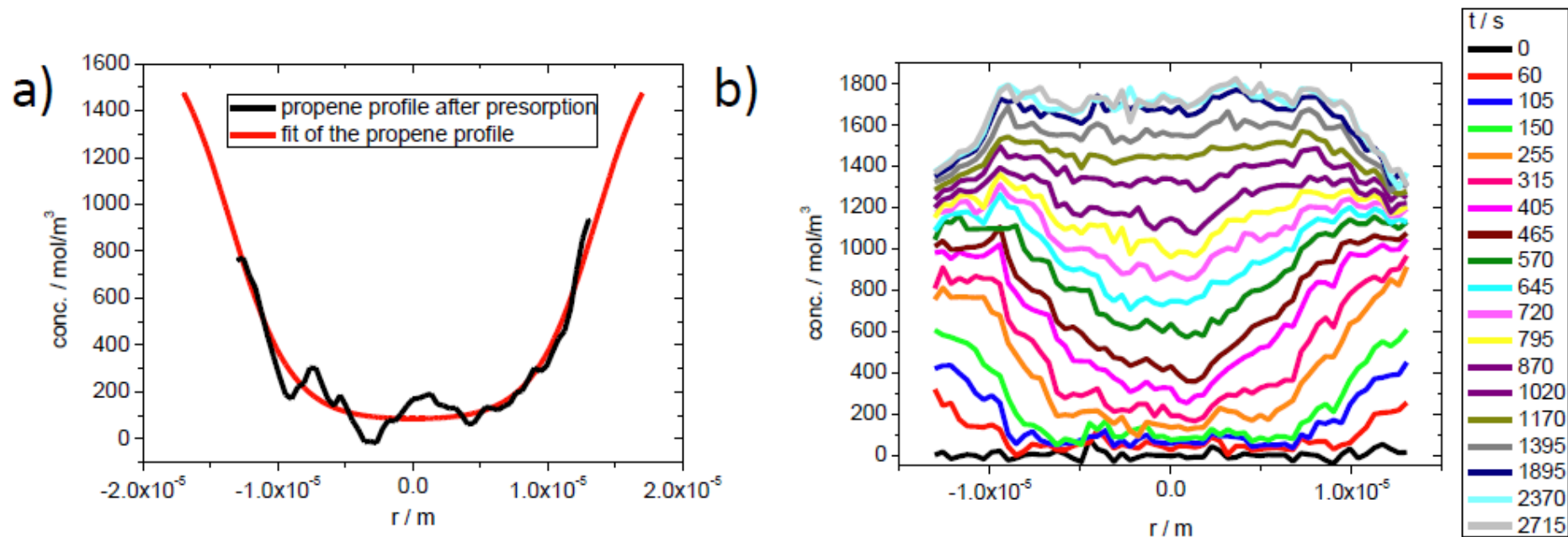
$$j_1 = -D_{11} \frac{\partial c_1}{\partial x} - D_{12} \frac{\partial c_2}{\partial x}$$

**Generalized Fick's 1st Law**

**Flux of component 1 is pushed  
 by concentration gradients of components 1 AND 2!**



# Evolution of Ethane Concentration in DDR after Propene Pre-Adsorption

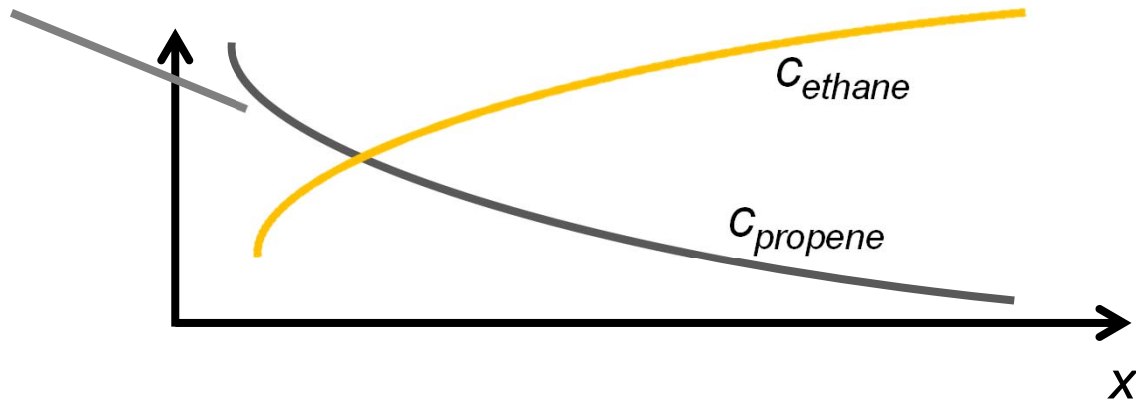
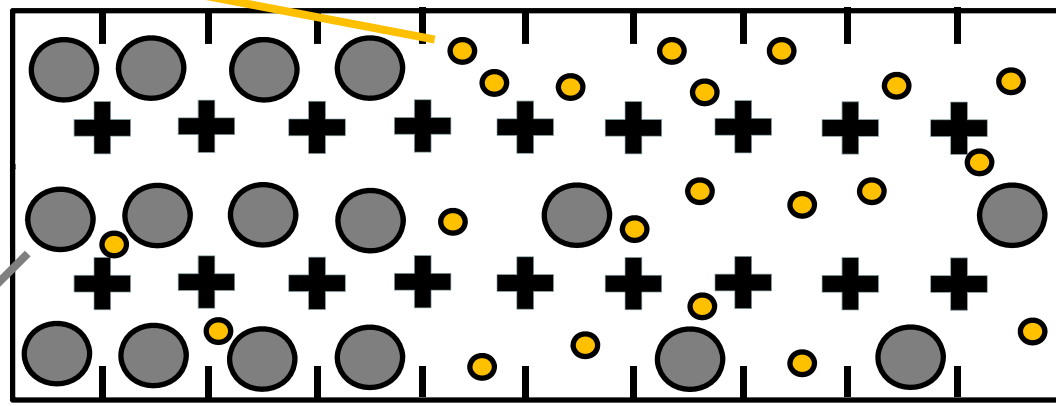
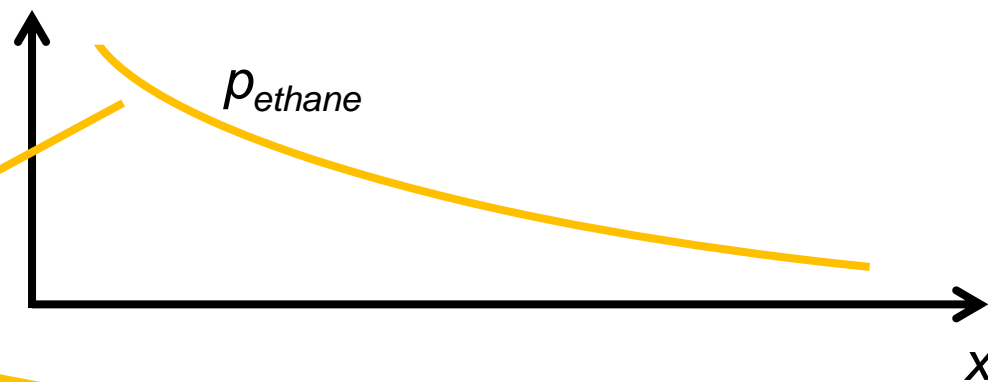


$$j_{ethane} = -D_{11} \frac{\partial c_{ethane}}{\partial x} - D_{12} \frac{\partial c_{propene}}{\partial x}$$

Back to the roots: Mass transfer is driven by gradient in chemical potential (and thus in pressure) of considered species rather than by (only) the concentration of this species

$$j_{ethane} \propto \frac{\partial \mu_{ethane}}{\partial x} \propto \frac{\partial \ln p_{ethane}}{\partial x}$$

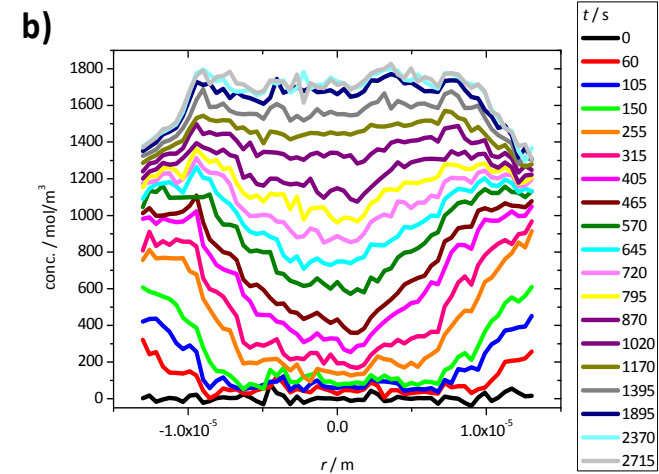
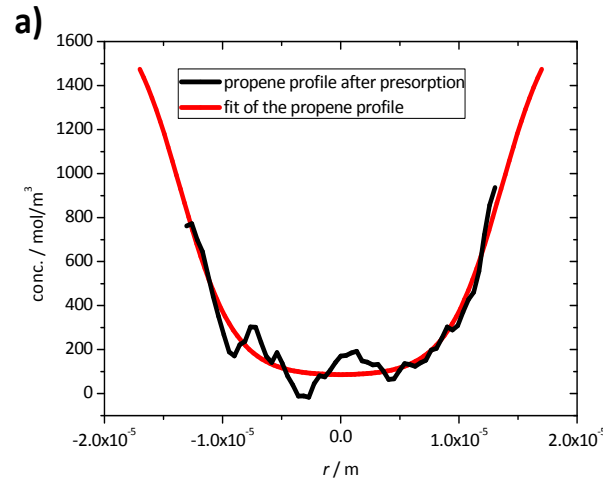
# Uphill Diffusion and Overshooting



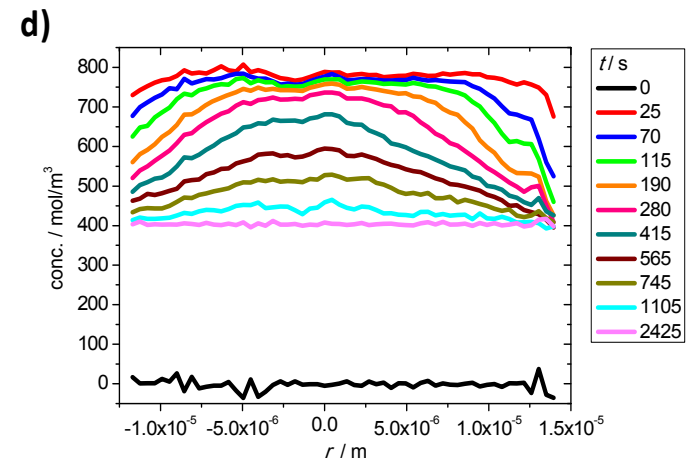
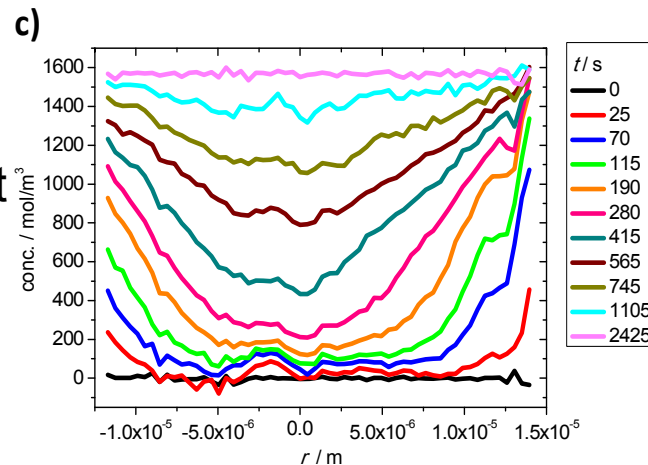
# Uphill Diffusion and Overshooting

Decreasing propene concentration pushes ethane „uphill“

Propene with Ethane as the „fast“ component



Ethane as the „slow“ component with CO<sub>2</sub>



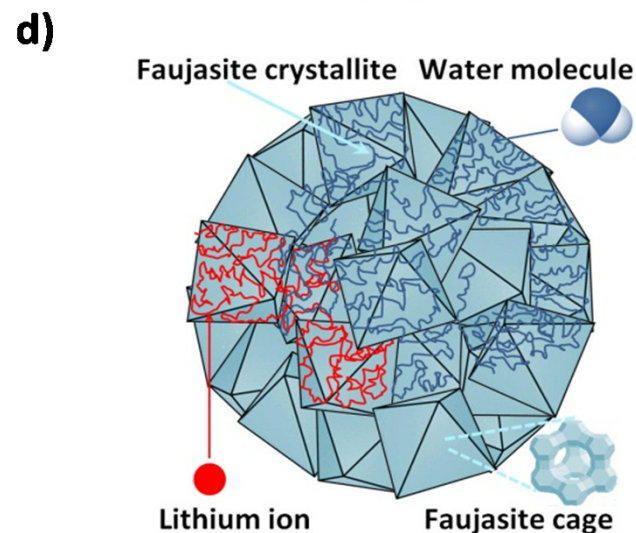
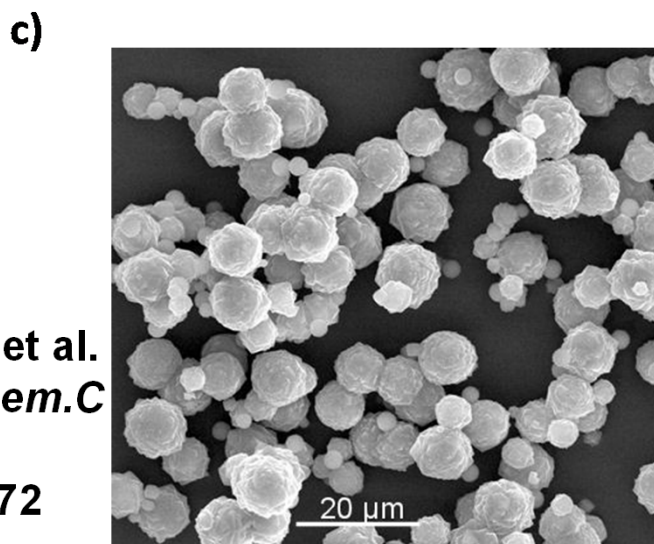
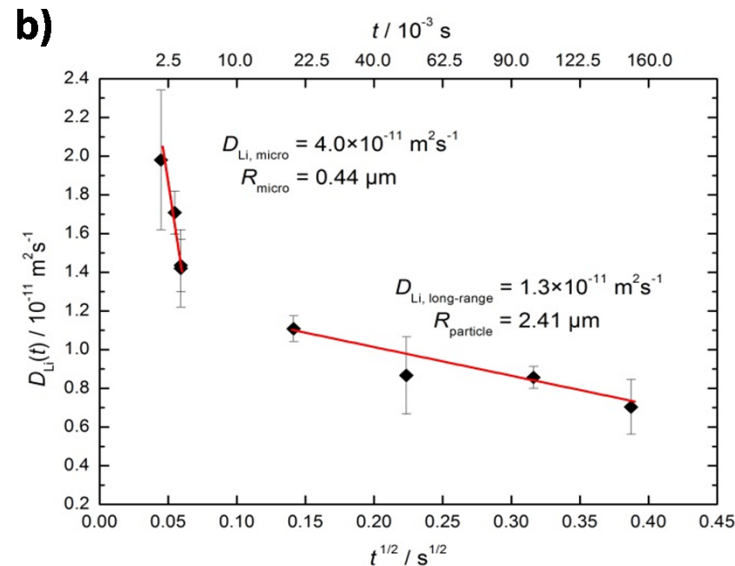
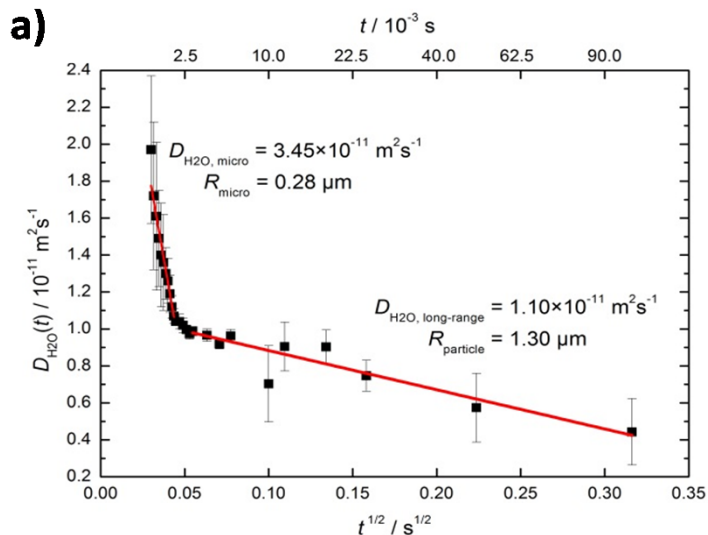
In parallel with ethane uptake and equilibration, CO<sub>2</sub> „overshoot“ is vanishing

A. Lauerer, T. Binder, C. Chmelik, E. Miersemann, J. Haase, D. M. Ruthven, J. Kärger, Nature Communications 6, 7697 (2015).

## **Contents:**

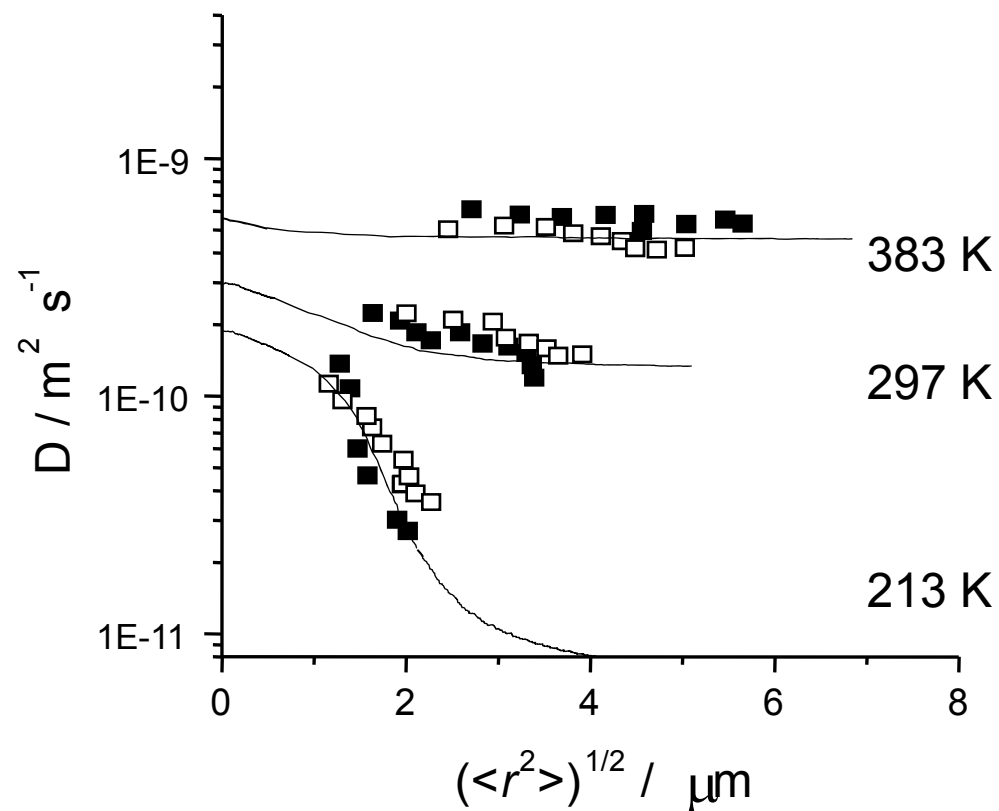
- 1) Tracing the diffusion path: PFG NMR diffusion measurement
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# Evidence of Internal Barriers by Time-Dependent PFG NMR Diffusivities of Water (a) at 25° C and of lithium cations (b) at 100 °C in hydrated zeolite Li-LSX

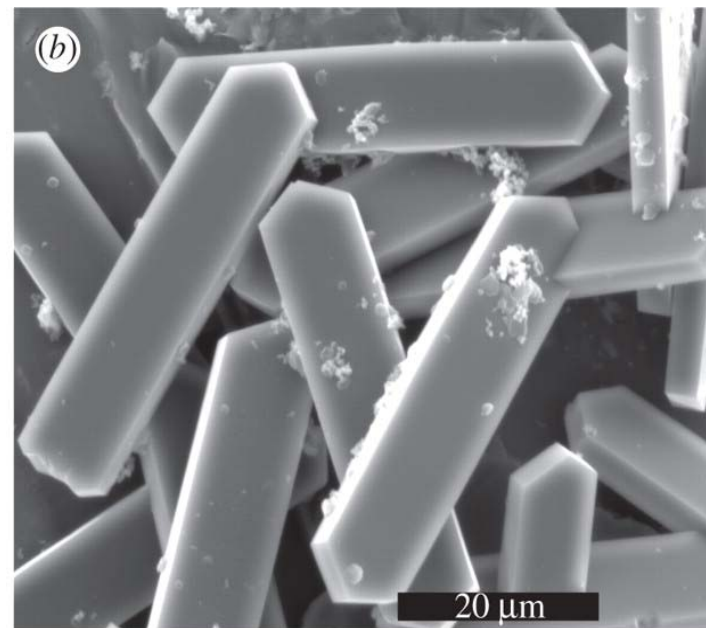


S. Beckert et al.  
*J. Phys.Chem.C*  
 2013, 117,  
 24866–24872

# Evidence of Intracrystalline Barriers by PFG NMR Diffusivities in seemingly perfect crystals



n-Butane / Silicalite-1



yielding an effective intracrystalline diffusivity

$$\frac{1}{D_{eff}} \approx \frac{1}{D} + \frac{1}{\alpha l}$$

with  $\alpha$  and  $l$  denoting the permeability and spacing of the intracrystalline barriers

**S. Vasenkov and J. Kärger,  
Microporous Mesoporous Mat.  
55, 139 (2002).**

**Medical diagnosis has attained such a high level**

**that there scarcely exist any really healthy people.**



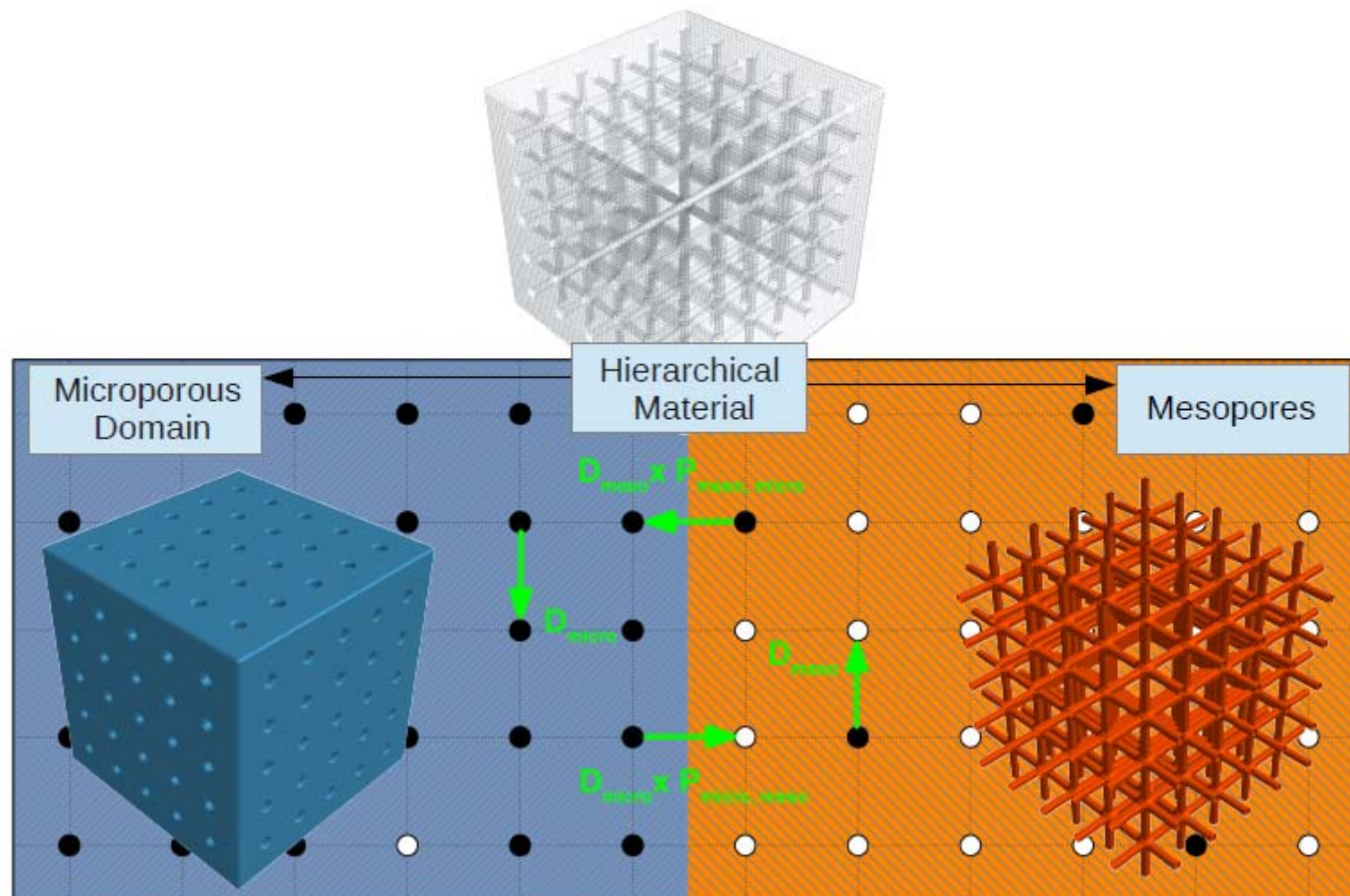
**Physical**

~~Medical~~ diagnosis has attained such a high level

**perfect crystals**

that there scarcely exist any really ~~healthy~~ ~~people~~.

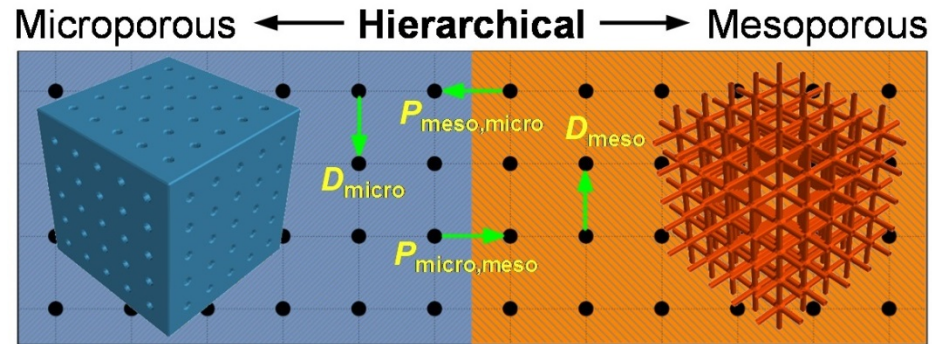
# „Highway“-Enhanced Mass Transfer in Microporous Materials



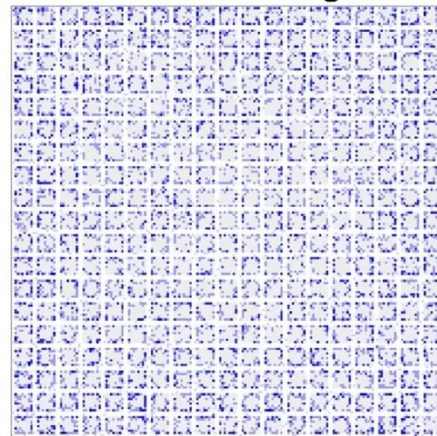
Schneider, D.; Kondrashova, D.; Valiullin, R.; Bunde, A.; Kärger, J. Chem. Ingen. Techn. submitted

Time constant of uptake and release by diffusion limitation:  $\tau_{\text{Diff}} = \frac{R^2}{15D}$ :

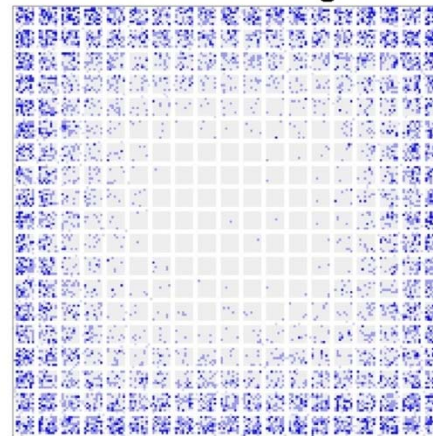
Transport Enhancement in Pore Hierarcies:



Slow exchange



Fast exchange



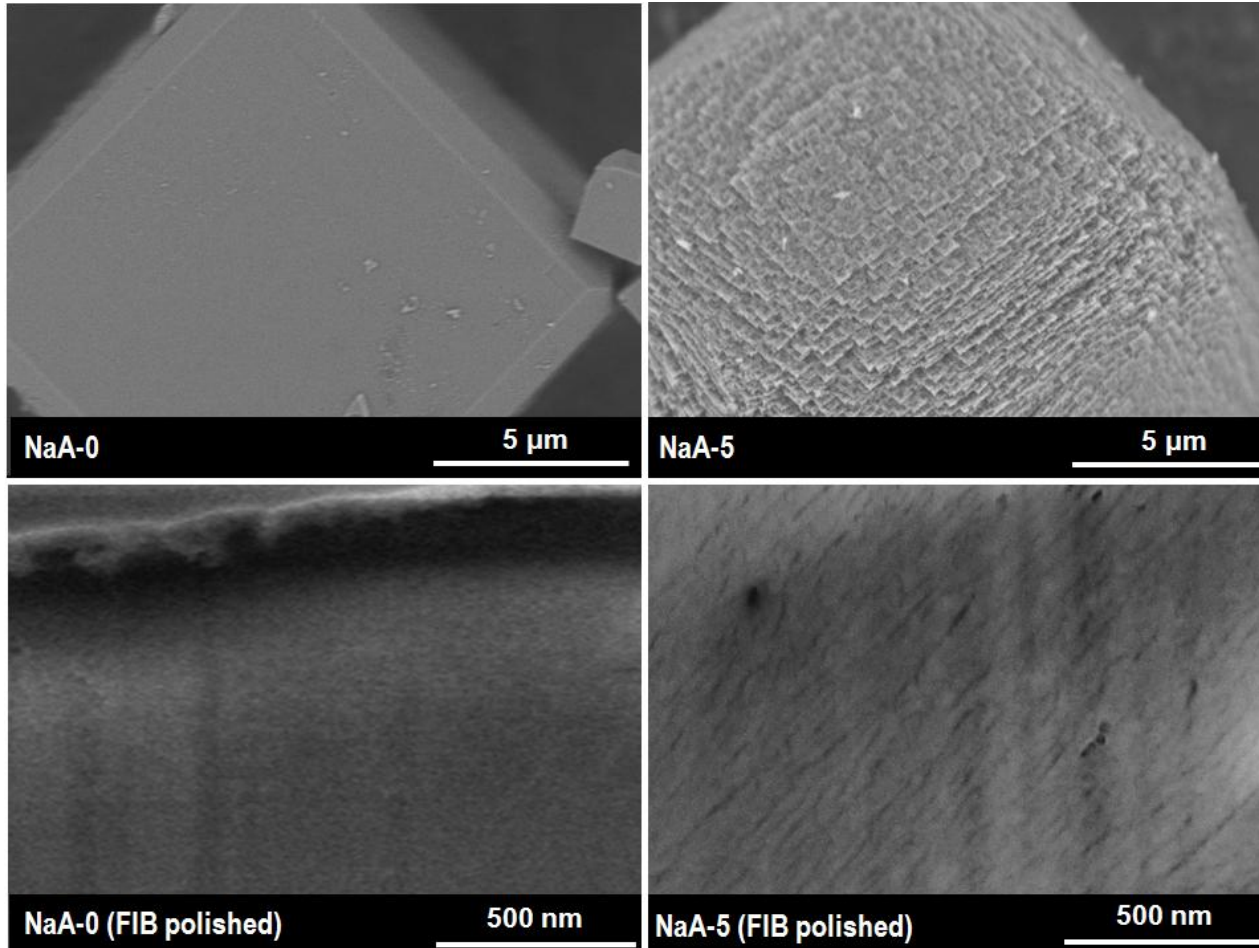
$$\tau_{\text{Diff}}^{\text{slow exchange}} = \frac{R_{\text{micro}}^2}{15D_{\text{micro}}} \quad \tau_{\text{Diff}}^{\text{fast exchange}} = \frac{R_{\text{cryst}}^2}{15(p_{\text{meso}}D_{\text{meso}} + D_{\text{micro}})}$$

Schneider, D.; Kondrashova, D.; Valiullin, R.; Bunde, A.; Kärger, J. Chem. Ingen. Techn. submitted

# Zeolite LTA

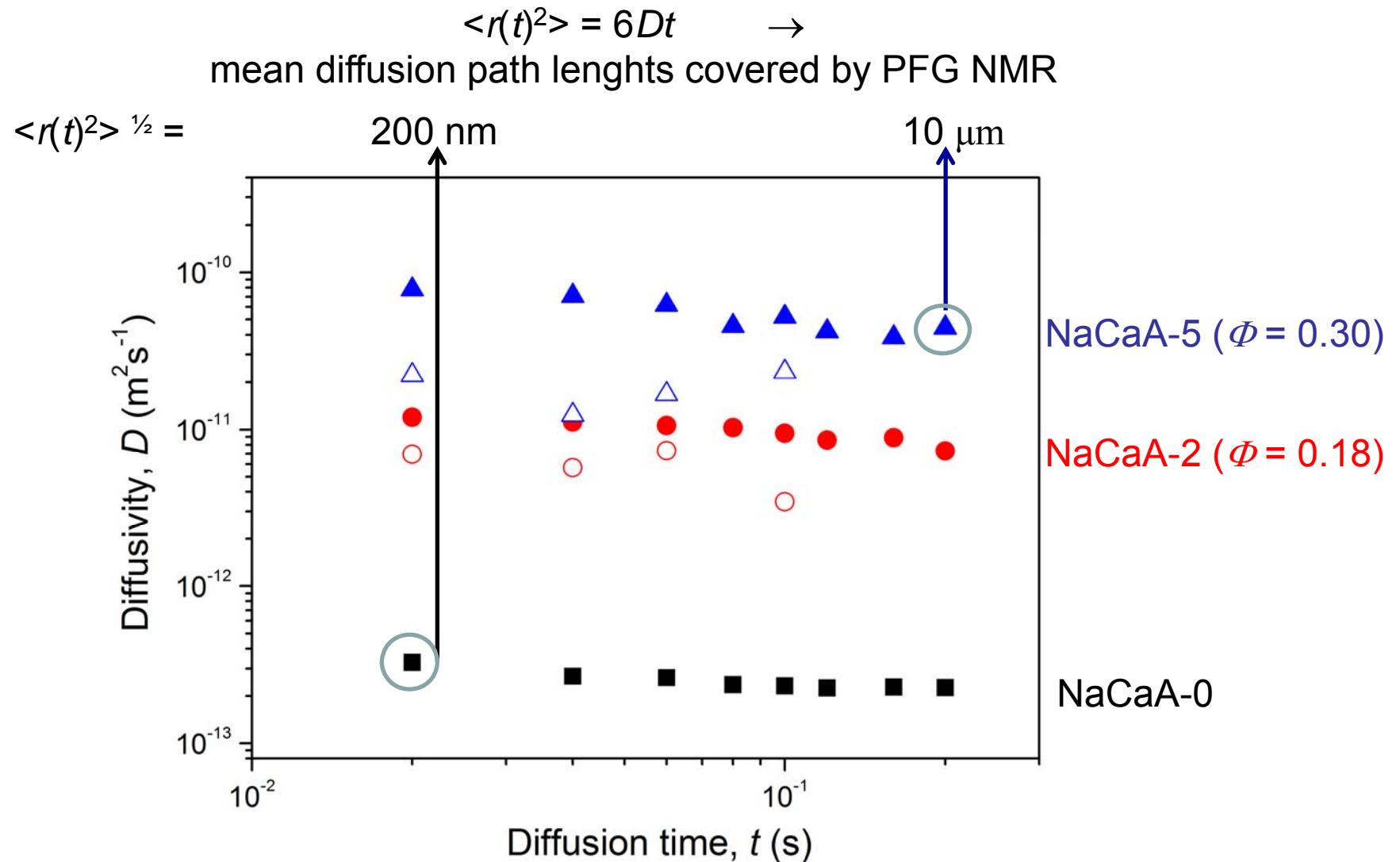
purely microporous

mesoporous



Mehlhorn, D.; Valiullin, R.; Kärger, J.; Cho, K.; Ryoo, R.:  
ChemPhysChem 13 (2012)1495-1499

# Propane Diffusivity in (mesoporous) Zeolite LTA at 25°C



D. Mehlhorn; R. Valiullin, J. Kärger, K. Cho, R. Ryoo, *ChemPhysChem* 13 1495 (2012)  
 J. Kärger, R. Valiullin, *Chem. Soc. Rev.* 42, 4172 (2013).

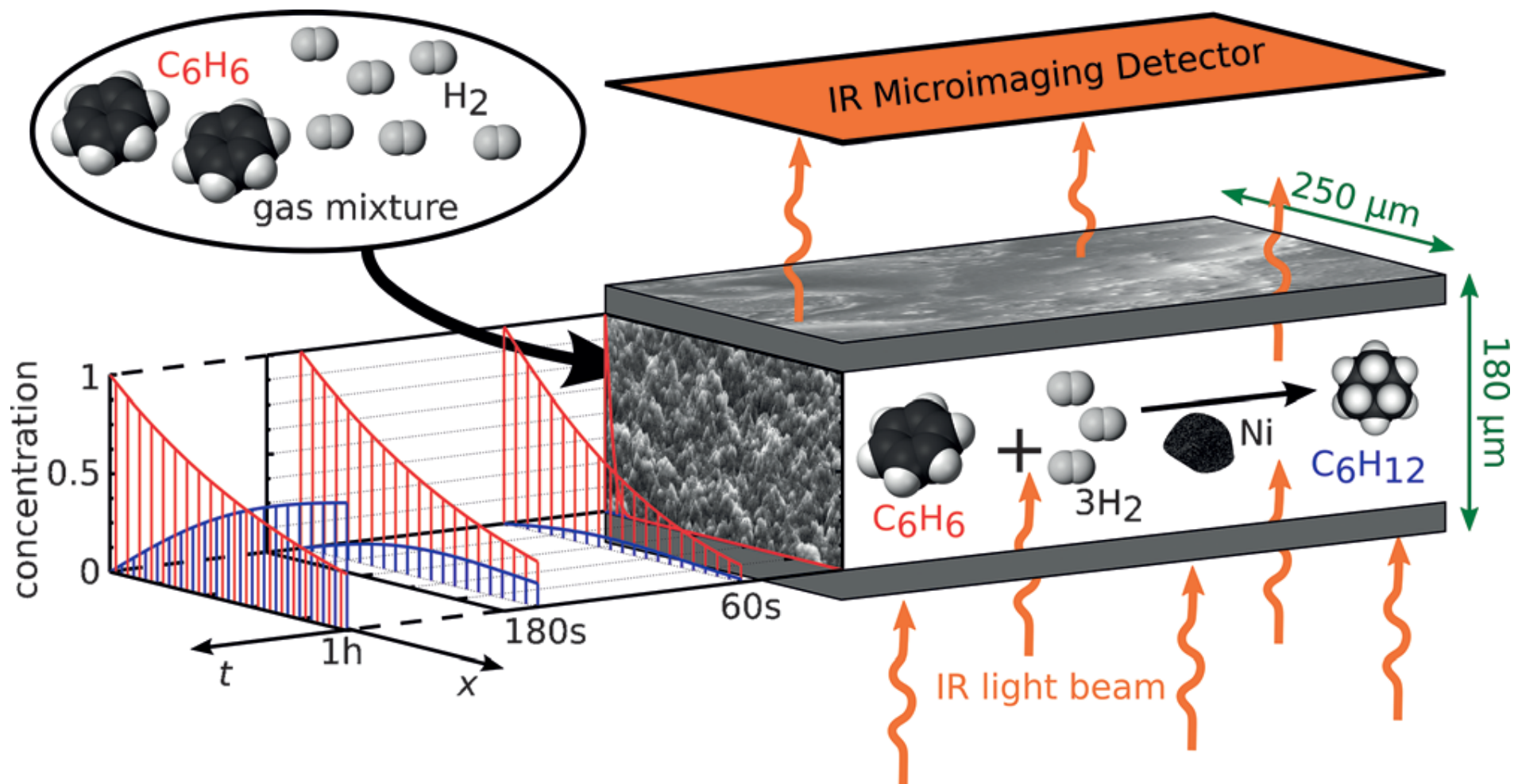


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# In-situ Recording of Chemical Reactions

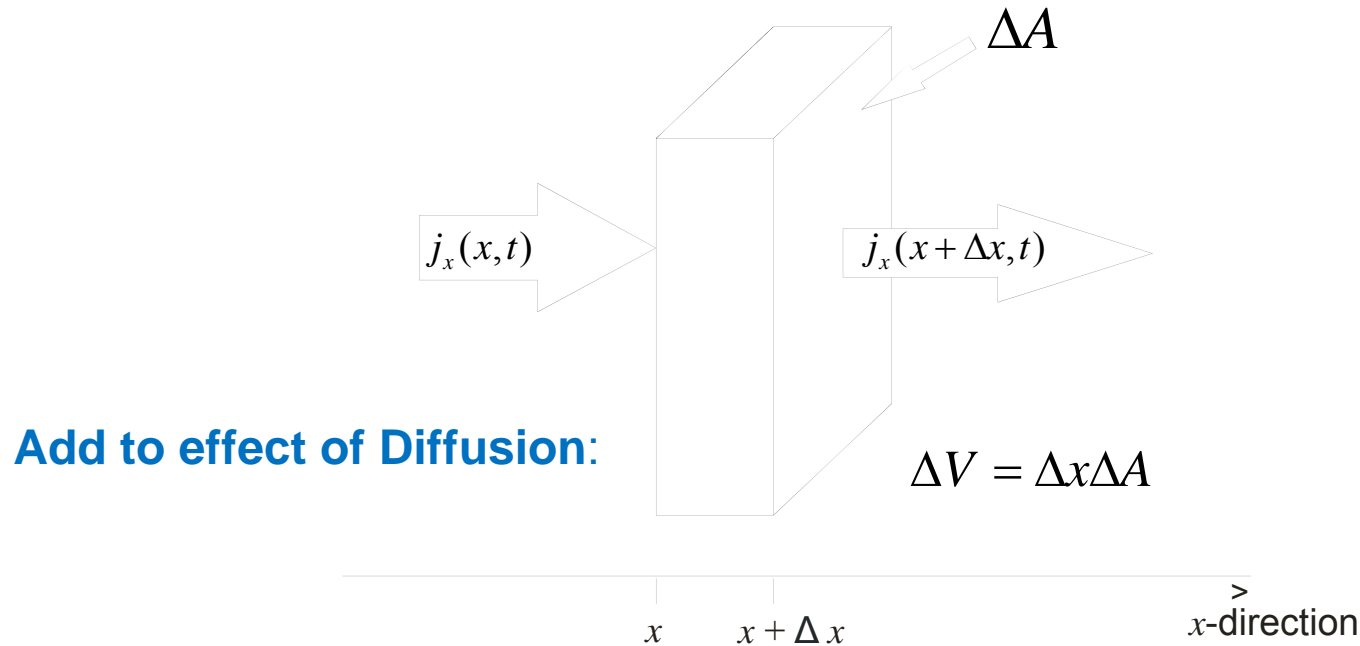
## Hydrogenation of Benzene to Cyclohexane



T. Titze *et al.*, *Angew. Chem. Int. Ed.* 54, 5060 (2015)



## Extending Fick's 2nd Law: Change of Concentration by Diffusion AND Conversion



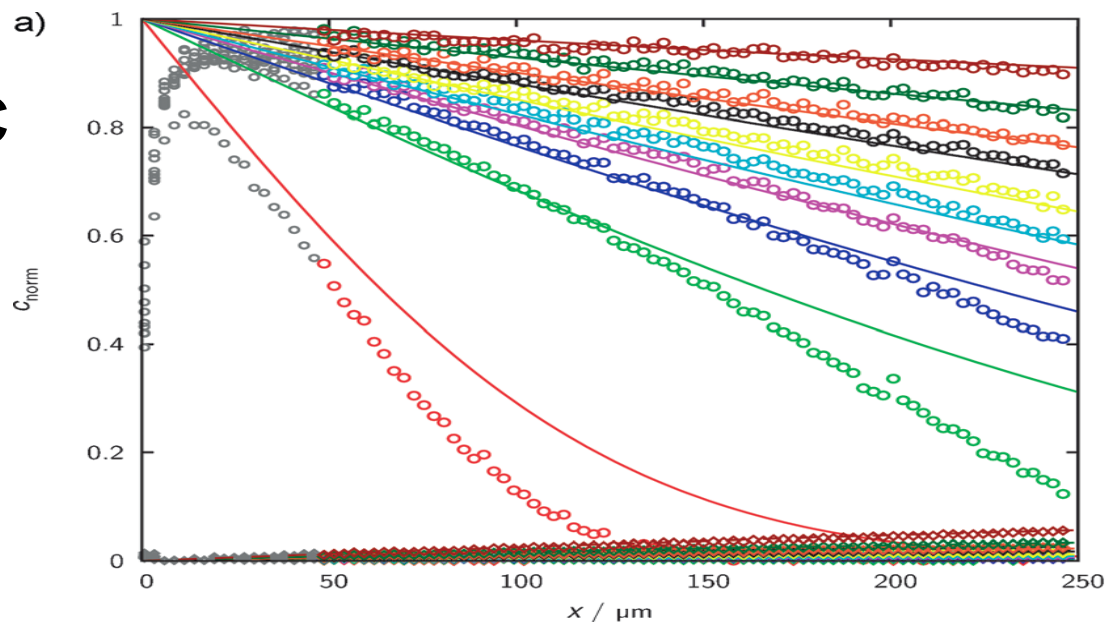
$$\begin{aligned} \frac{\partial c_1}{\partial t} &= \left( \frac{\partial c_1}{\partial t} \right)_{\text{Diffusion}} + \left( \frac{\partial c_1}{\partial t} \right)_{\text{Conversion}} \\ &= - \frac{\partial j_1}{\partial x} - k c_1 \\ &= D \frac{\partial^2 c_1}{\partial x^2} - k c_1 \end{aligned}$$

**effect of Conversion (reaction)**

**In our case:  
irreversible reaction  
from species 1 to 2**

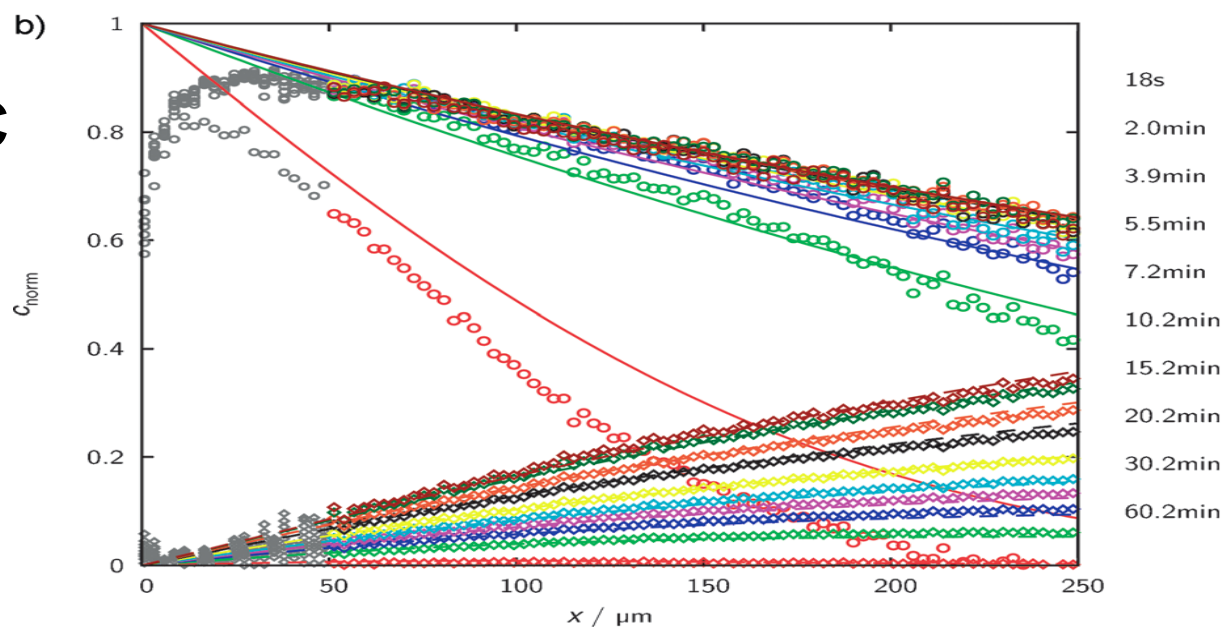
$$\frac{\partial c_2}{\partial t} = D \frac{\partial^2 c_2}{\partial x^2} + k c_1$$

25°C



Conversion from **Benzene** (top) to **Cyclohexane** (bottom) upon **uptake by a nanoporous glass** with dispersed Ni particles as a catalyst

75°C

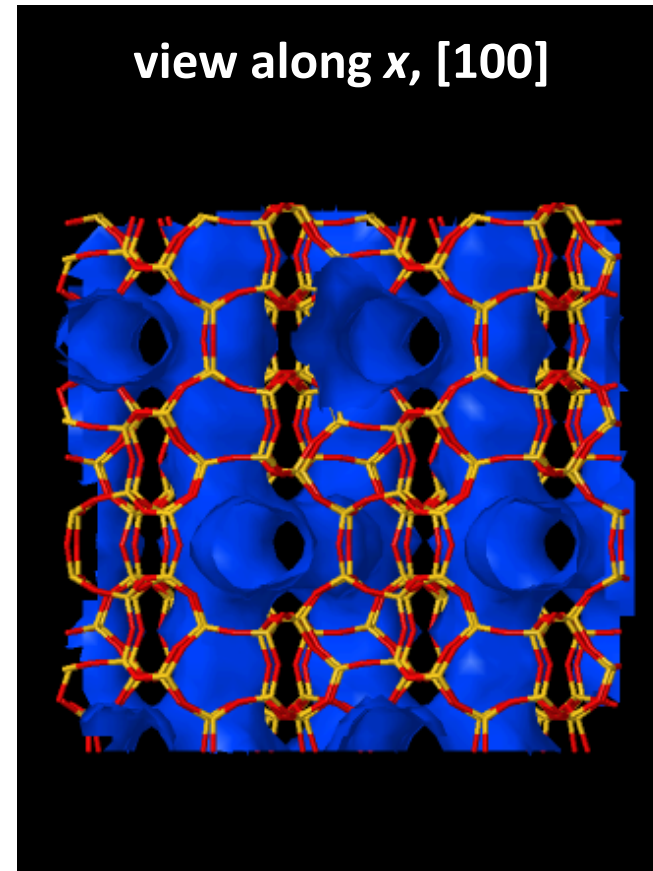
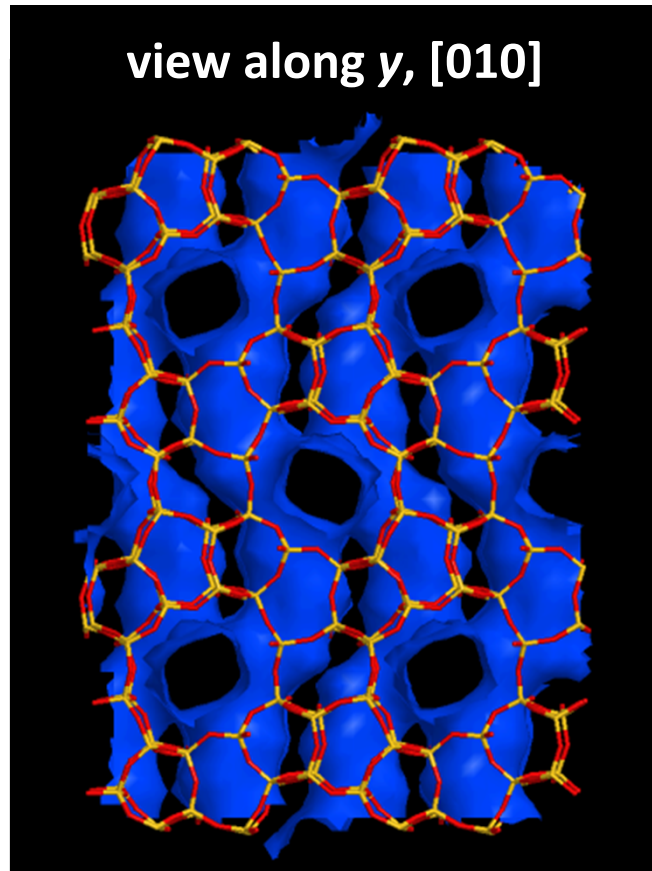


T. Titze *et al.*,  
Angew. Chem.  
Int. Ed. **54**, 5060  
(2015).

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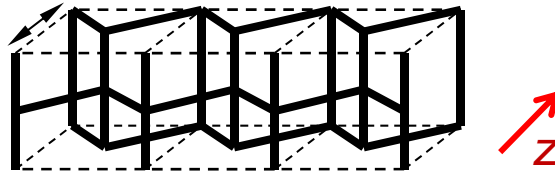
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# MFI-type structure – intersecting channels (3d)

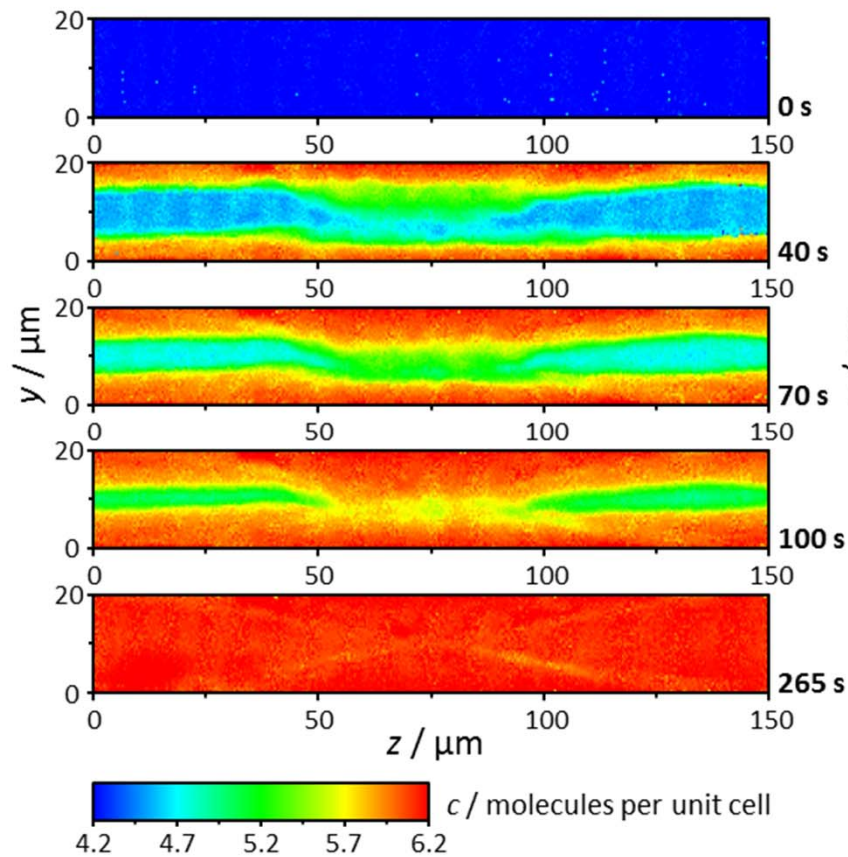


- 10-membered ring zigzag-channels ( $5.5 \times 5.1 \text{ \AA}^2$ ) along x [100]
- 10-membered ring straight channels ( $5.6 \times 5.3 \text{ \AA}^2$ ) along y [010]

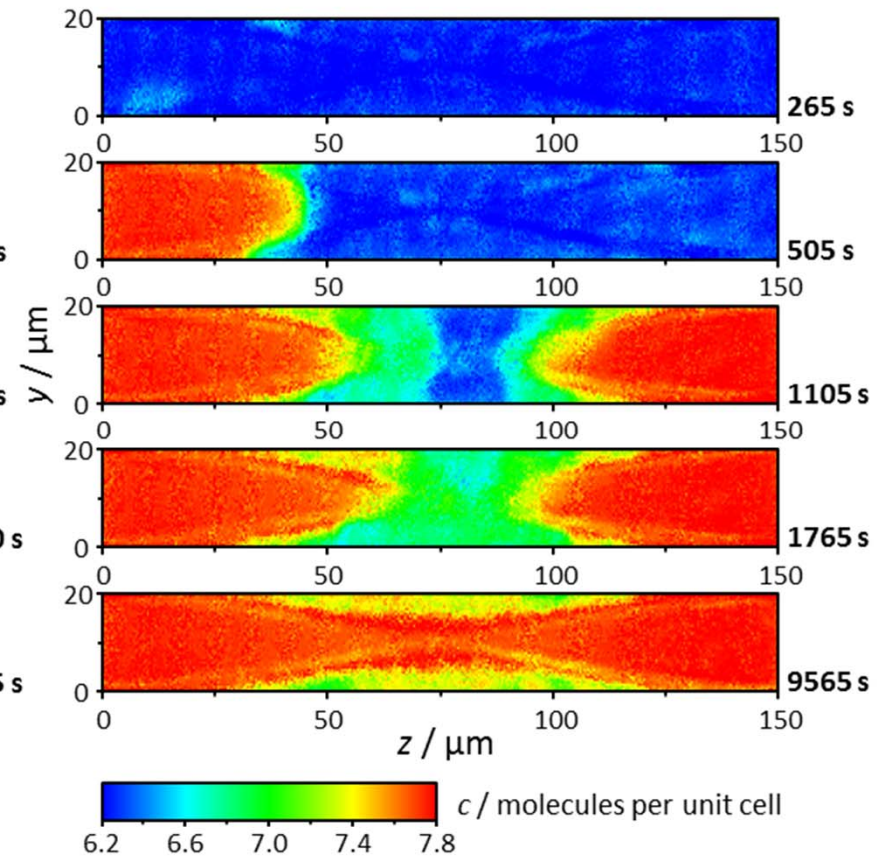
# Benzene adsorption in zeolite MFI, pressure step 0.5 to 1 kPa



1<sup>st</sup> step: profile evolution  
along channels



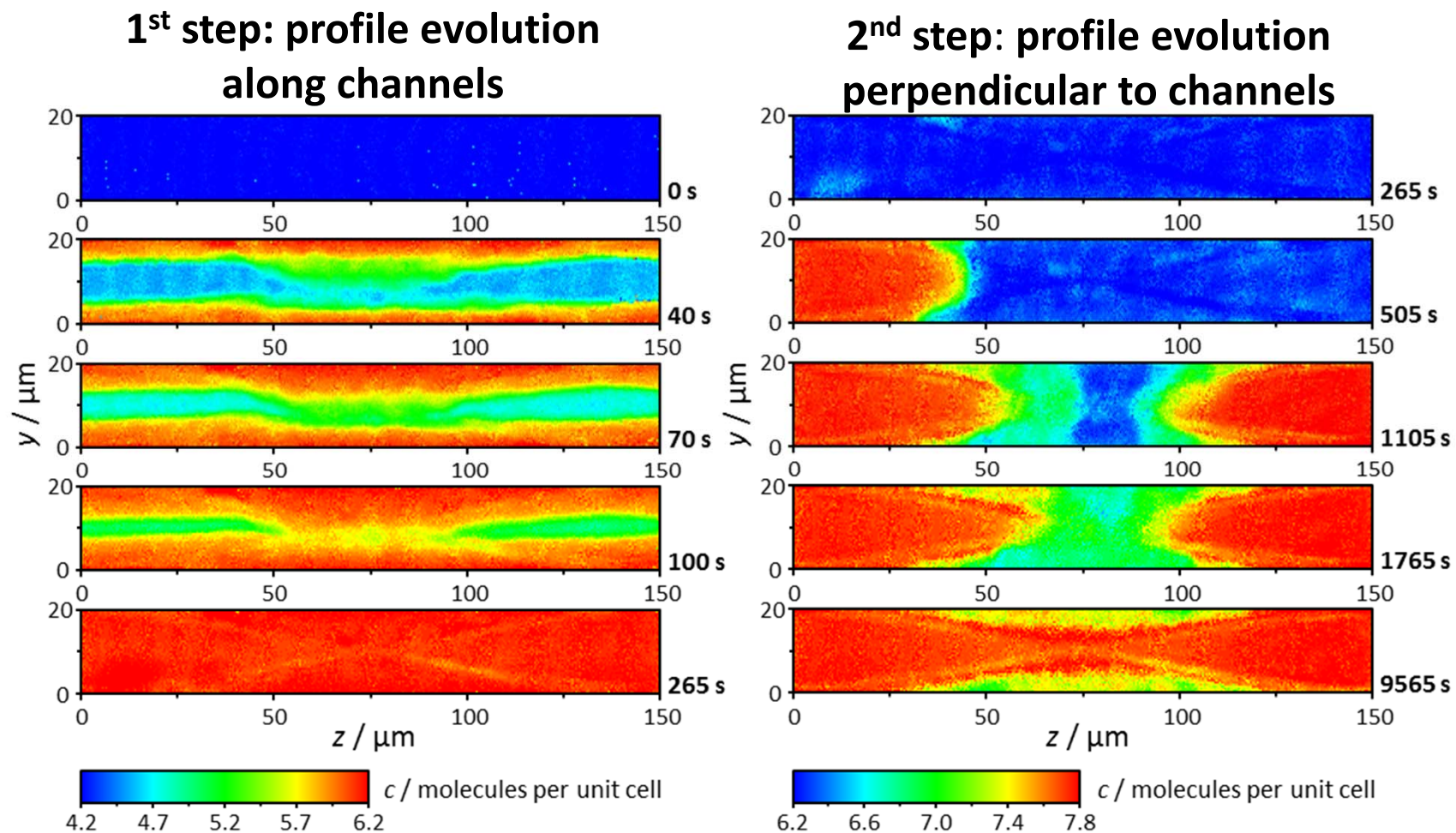
2<sup>nd</sup> step: profile evolution  
perpendicular to channels



J. Kärger, T. Binder, C. Chmelik, F. Hibbe, H. Krautscheid, R. Krishna, and J. Weitkamp, *Nature Materials* 13 (2014) 333–343



# Benzene adsorption in zeolite MFI, pressure step 0.5 to 1 kPa



**After a Couple of Minutes the Presence of the Guest starts to Change the Host, which takes a Couple of Hours**

J. Kärger, T. Binder, C. Chmelik, F. Hibbe, H. Krautscheid, R. Krishna, and J. Weitkamp, *Nature Materials* 13 (2014) 333–343



# Molecules Spreading in Pore Spaces

- **Observation of Molecular Spreading**
- **Infestation of New Territories**
- **Interaction between Invaders of One and Various Species**
- **The Driving Force of Infestation**
- **Barriers and Highways**
- **Conversion of Invadors during Invasion**
- **Invadors-Induced Changes of the Territory**

# Molecules Spreading in Pore Spaces

- Observation of Molecular Spreading
- Infestation of New Territories
- Interaction between Invaders of One and Various Species
- The Driving Force of Infestation
- Barriers and Highways
- Conversion of Invaders during Invasion
- Invaders-Induced Changes of the Territory

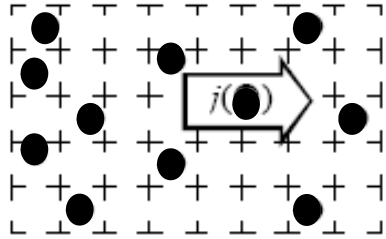
**Surprises  
may be Hidden  
Anywhere**



- 
- Optional, if needed for discussion:

# Correlating Diffusion under Equilibrium and Non-Equilibrium

- Transport (Collective, Chemical) Diffusion

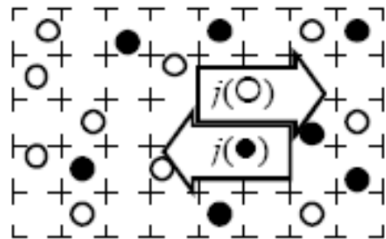


$$j_x = -D_T \frac{\partial c}{\partial x}$$

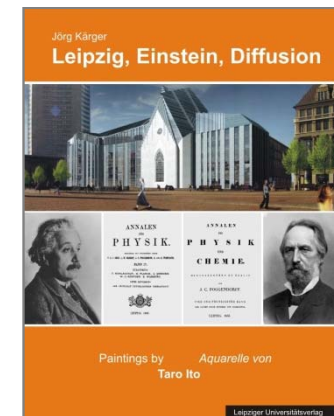
**(Fick's 1<sup>st</sup> law)**



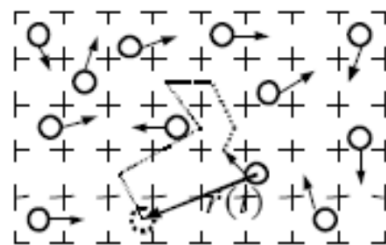
- Self- (Tracer) Diffusion by Tracer Exchange



$$j_x^* = -D \frac{\partial c^*}{\partial x}$$

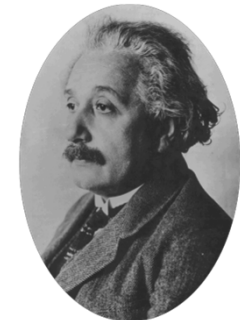


- Self- (Tracer) Diffusion by Following the Individual Molecules (QENS, PFG NMR)

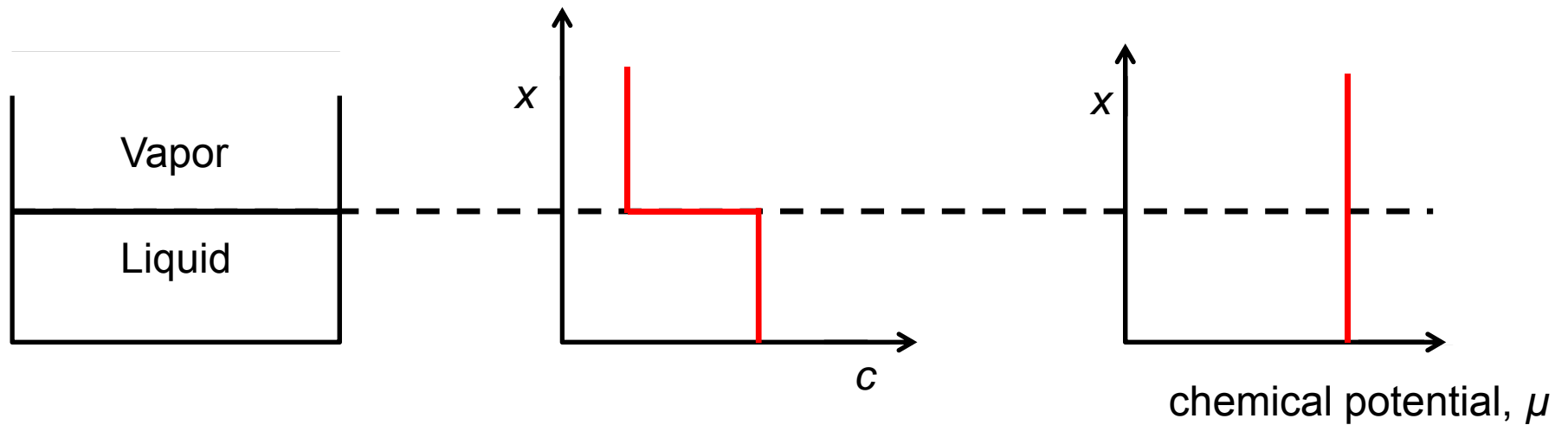


$$\langle x^2(t) \rangle = 2Dt$$

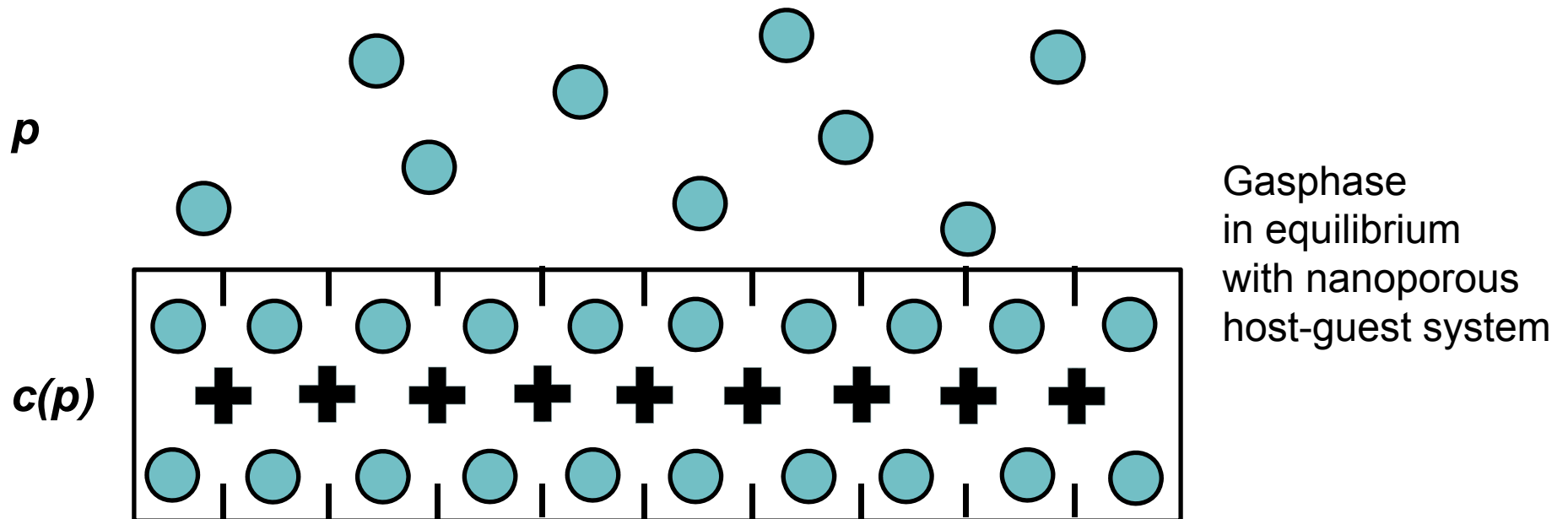
**Einstein Equation**



# Driving Force of Diffusion

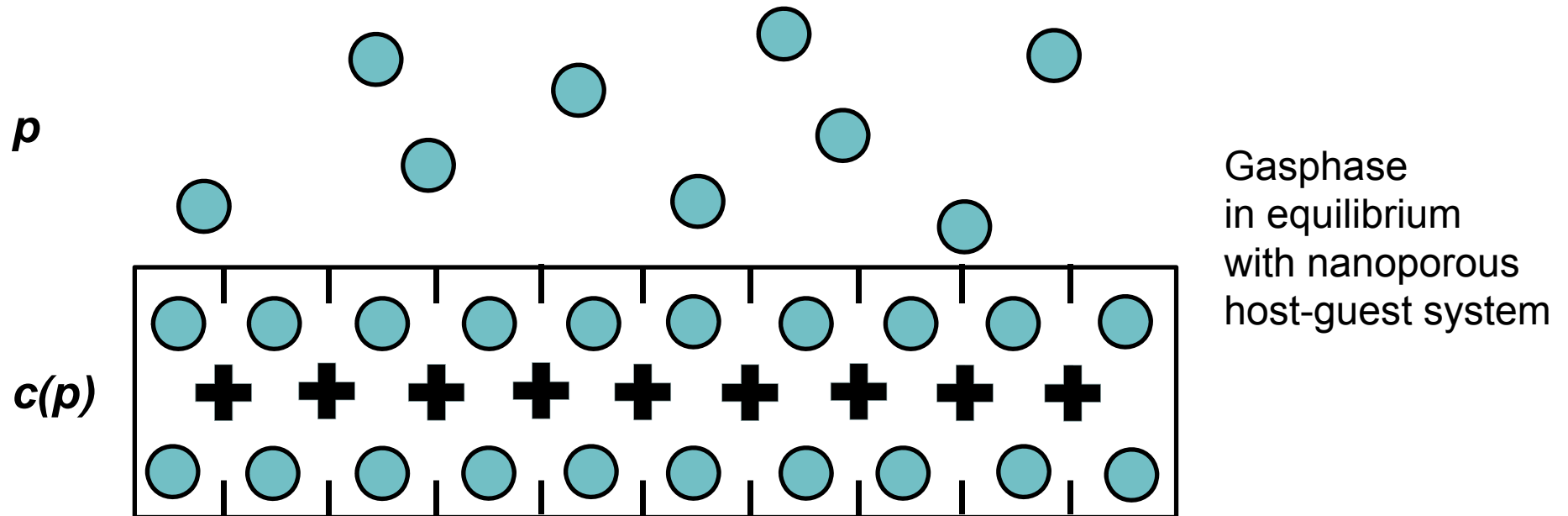


$$\mu = RT \ln p_{equilibrium}$$





# Driving Force of Diffusion



Single-component host-guest system

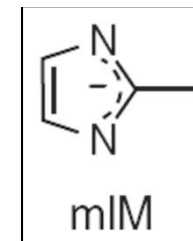
$$j \propto c \frac{\partial \mu}{\partial x} \propto c \frac{\partial \ln p}{\partial x} \propto c \frac{\partial \ln p(c)}{\partial c} \frac{\partial c}{\partial x} = \frac{\partial \ln p(c)}{\partial \ln c} \frac{\partial c}{\partial x}$$

yields Fick's 1st law

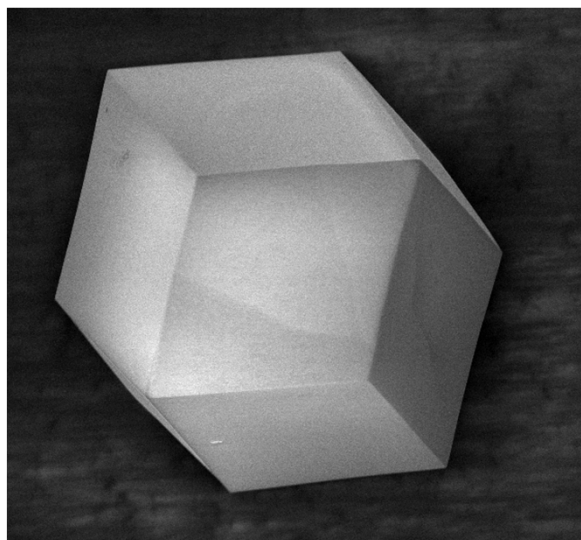
$$j = \text{concentration dependent factor} \times \frac{\partial c}{\partial x}$$

# Our Probe System

MOFs (Metal-Organic Frameworks) of type ZIF: Zeolitic Imidazolate Frameworks (ZIF-8  $\leftrightarrow$  SOD)

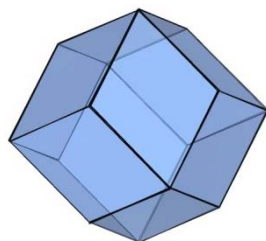


SEM image (J. Caro)

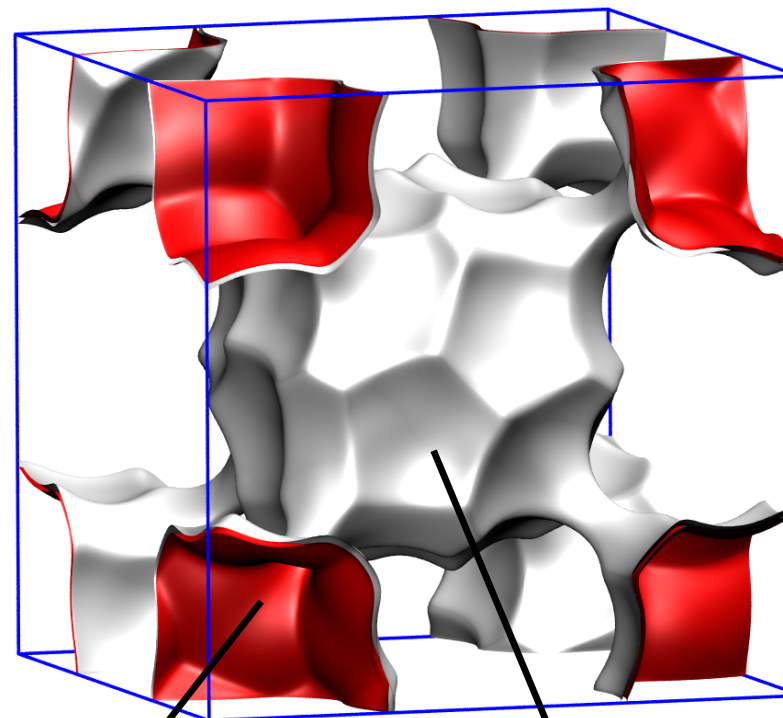


crystal size: up to 300  $\mu\text{m}$

crystal shape: rhombic dodecahedron



potential landscape (R. Krishna)



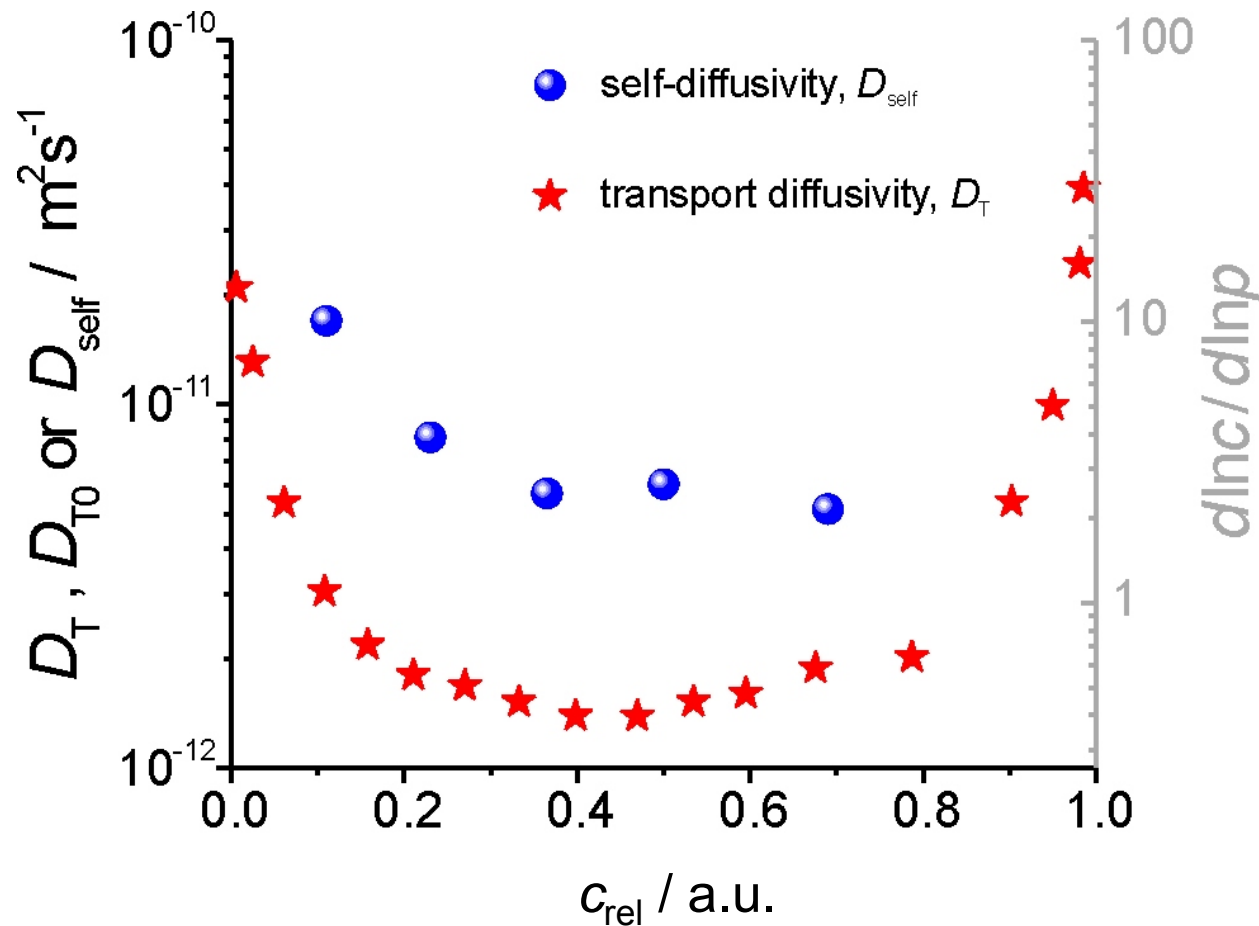
window size:  
ca. 3.4  $\text{\AA}$

cavity size: ca. 12  $\text{\AA}$

unit cell:  $a = b = c \approx 17 \text{\AA}$

in collaboration with J. Caro, Hannover

# Methanol in ZIF-8

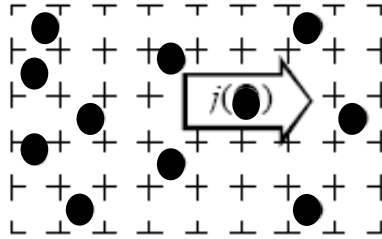


- $D_{\text{self}} > D_{\text{T}}$ : Faster by opposing the stream?

C. Chmelik, H. Bux, J. Caro, L. Heinke, F. Hibbe, T. Titze, and J. Kärger; “Mass Transfer in a Nanoscale Material Enhanced by an Opposing Flux”, *Phys. Rev. Lett.* 104 (2010) 085902.

# Equilibrium versus Non-Equilibrium

- Transport (Collective, Chemical) Diffusion

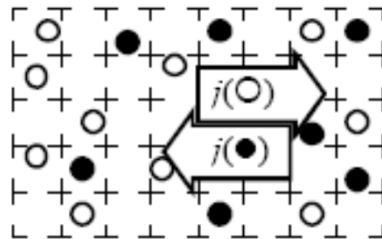


$$j_x = -D_T \frac{\partial c}{\partial x}$$

(Fick's 1<sup>st</sup> law)



- Self- (Tracer) Diffusion by Tracer Exchange



$$j_x^* = -D \frac{\partial c^*}{\partial x}$$

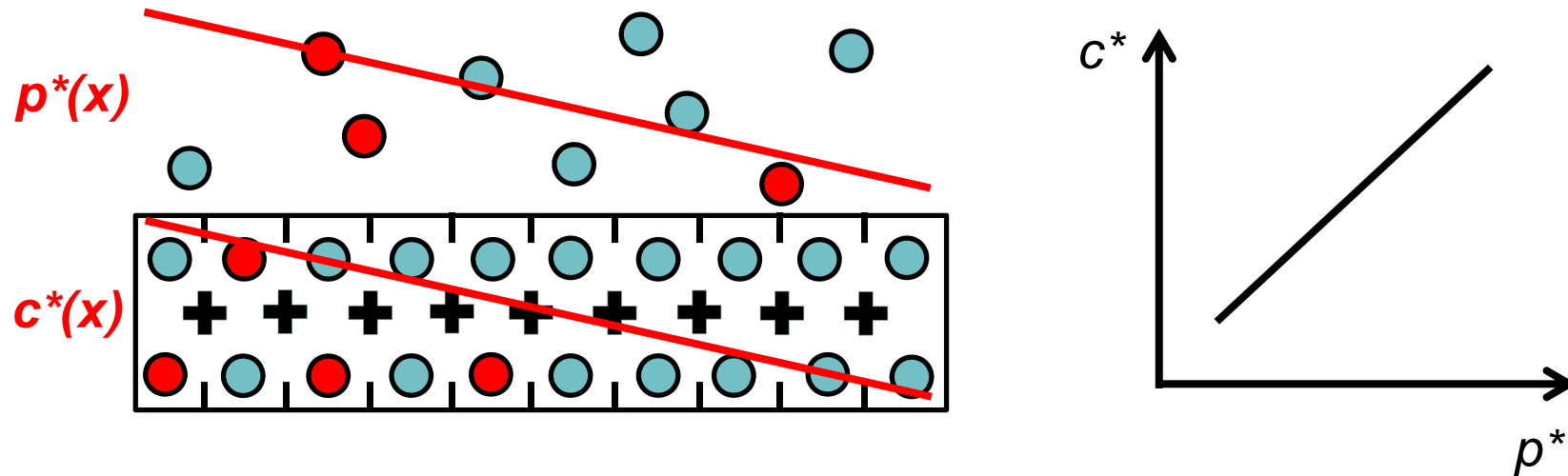


$$j \propto c \frac{\partial \mu}{\partial x} \propto c \frac{\partial \ln p}{\partial x} \propto c \frac{\partial \ln p(c)}{\partial c} \frac{\partial c}{\partial x} = \frac{\partial \ln p(c)}{\partial \ln c} \frac{\partial c}{\partial x} = \frac{\partial p / \partial c}{p/c} \frac{\partial c}{\partial x}$$

Implying identical concentration gradients  
we may thus note:

$$\frac{D^*}{D_T} = \frac{j^*}{j} = \frac{\partial \ln p^*}{\partial \ln c^*} / \frac{\partial \ln p}{\partial \ln c}$$

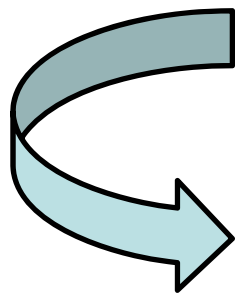
# Tracer Diffusion



## Equilibrium

$$j \propto c \frac{\partial \mu}{\partial x} \propto c \frac{\partial \ln p}{\partial x} \propto c \frac{\partial \ln p(c)}{\partial c} \frac{\partial c}{\partial x} = \frac{\partial \ln p(c)}{\partial \ln c} \frac{\partial c}{\partial x} = \frac{\partial p / \partial c}{p/c} \frac{\partial c}{\partial x}$$

Tracer (or Self-) Diffusion:  $\frac{\partial p^*}{\partial c^*} = \frac{p^*}{c^*}$



$$\frac{D_T}{D^*} = \frac{j}{j^*} = \frac{\frac{\partial \ln p(c)}{\partial \ln c}}{1}$$



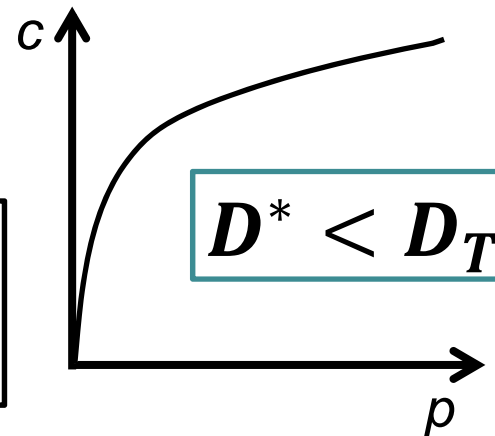
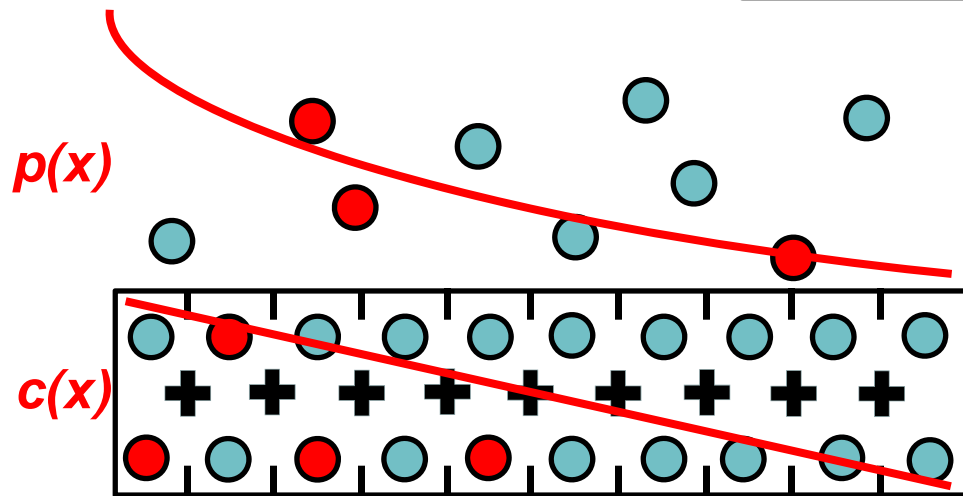
$$D^* = D_T \frac{\partial \ln c}{\partial \ln p} = D_T \frac{\partial c / \partial p}{c/p}$$



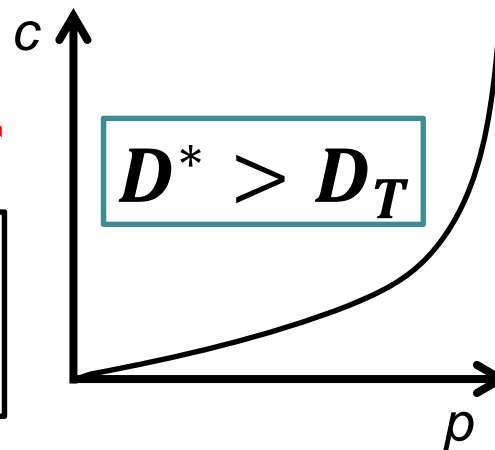
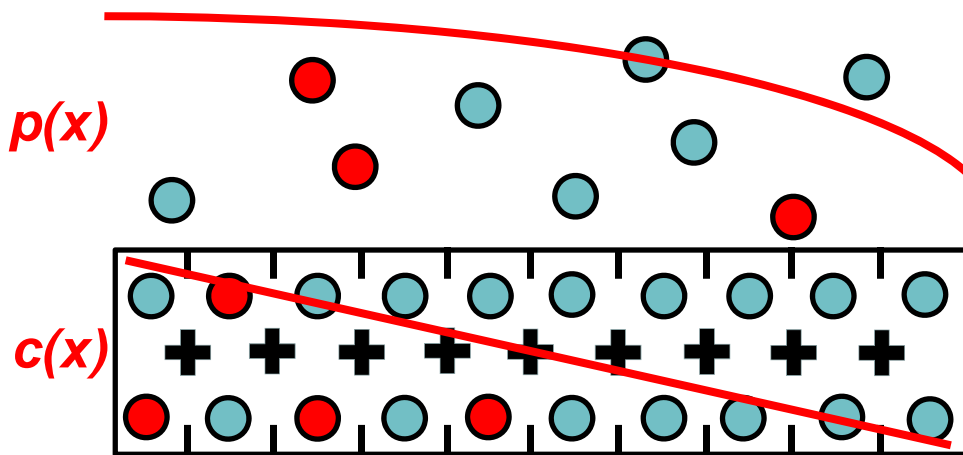
# Non-Equilibrium

$$D^* = D_T \frac{\partial \ln c}{\partial \ln p} = D_T \frac{\partial c / \partial p}{c/p}$$

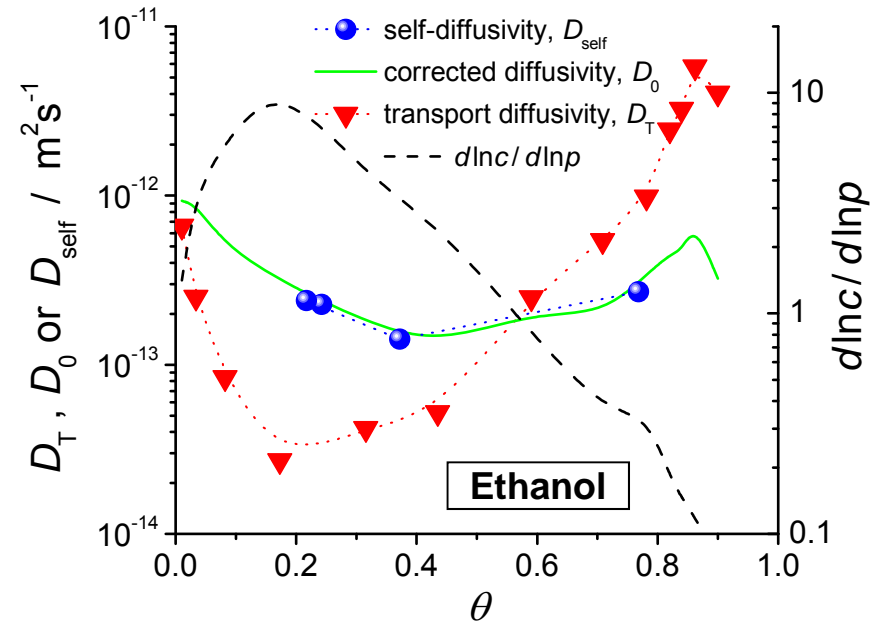
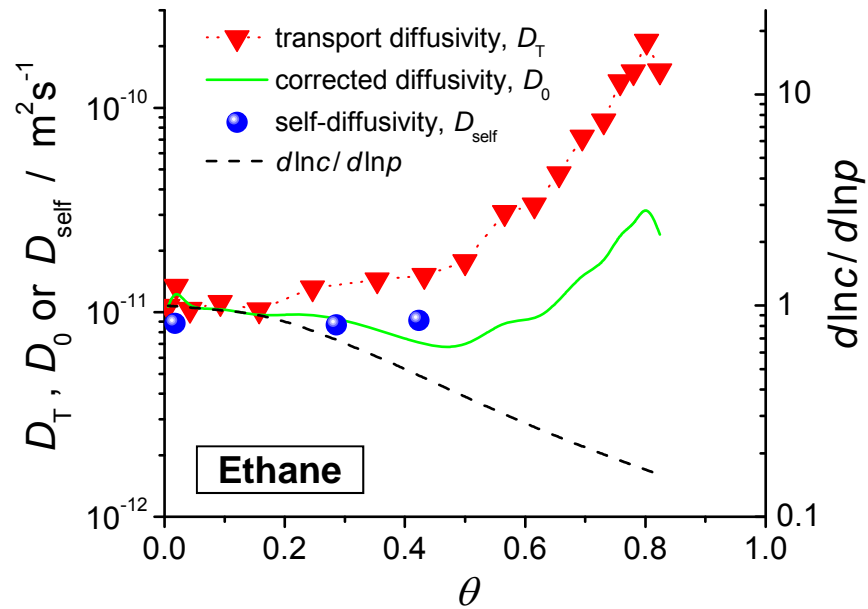
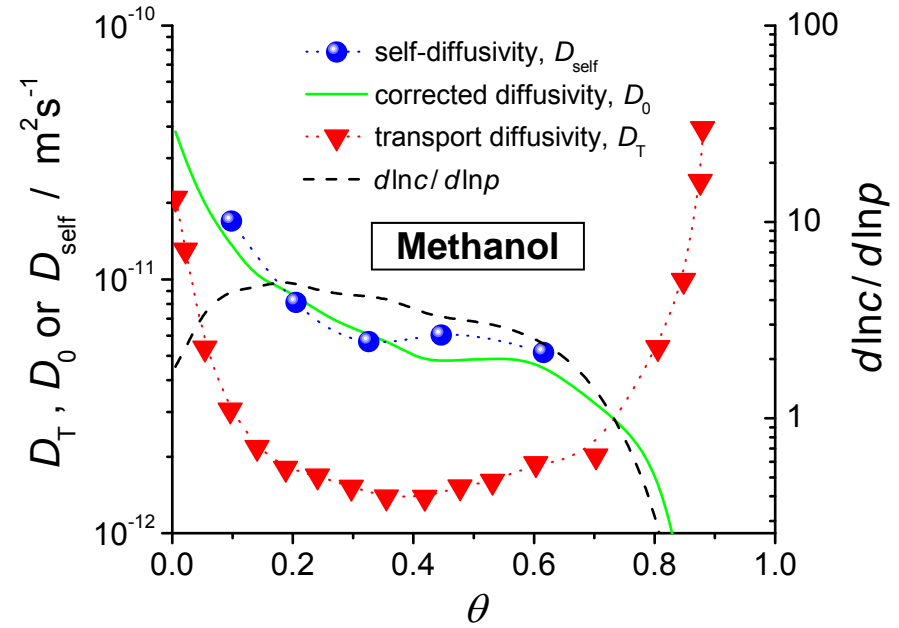
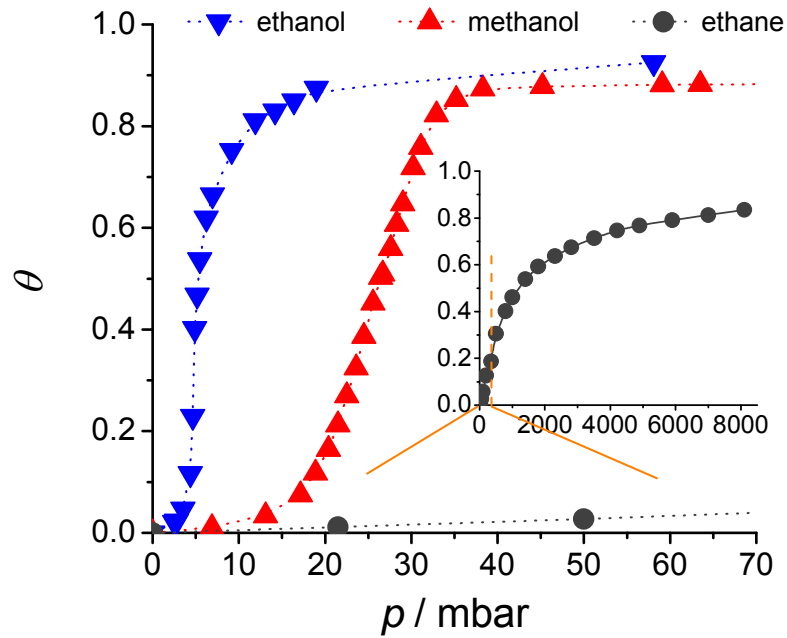
Competitive Adsorption



Mutual Attraction



# Methanol, Ethanol and Ethane in ZIF-8



# Methanol, Ethanol and Ethane in ZIF-8

## Unique experimental proofs:

- $D_{\text{self}} = D_0 = D_T$  for  $c \rightarrow 0$
- Correlating equilibrium and non-equilibrium quantities
- $D_{\text{self}} > D_T$  possible

